

**SECTION - A**There are **FOUR** questions in this section. Answer any **THREE**.

Symbols used have their usual meaning.

1. (a) Using elementary row operations compute the inverse of the following matrix
- (24  $\frac{2}{3}$ )

$$A = \begin{bmatrix} 1 & -1 & 0 & 0 \\ 1 & 2 & 0 & 0 \\ -6 & 0 & 1 & -2 \\ 8 & 1 & -2 & 1 \end{bmatrix}$$

- (b) Find the eigenvalues and the corresponding eigenvectors of the matrix
- (22)

$$A = \begin{bmatrix} 5 & 3 & -1 \\ 3 & 5 & -1 \\ -3 & -3 & 3 \end{bmatrix}$$

2. (a) Reduce
- $A = \begin{bmatrix} 1 & -2 & 1 & 3 \\ 4 & -1 & 5 & 8 \\ 2 & 3 & 3 & 2 \end{bmatrix}$
- to the normal form B and compute the matrices P and

Q such that  $PAQ = B$ , where A and B are equivalent matrices. (22)

- (b) Reduce the quadratic form
- $x_1^2 + 2x_2^2 + 3x_3^2 + 4x_1x_2 + 10x_2x_3 + 6x_3x_1$
- to the canonical form and find the corresponding linear transformation, rank, index and signature of the form.
- (24  $\frac{2}{3}$ )

3. (a) Find the equation of the tangent plane and normal line to the surface
- $4z = x^2 - y^2$
- at the point (3, 1, 2).
- (15)

- (b) Show that
- $\vec{\nabla} \times (\phi \vec{A}) = \phi (\vec{\nabla} \times \vec{A}) + (\vec{\nabla} \phi) \times \vec{A}$
- , hence find
- $\vec{\nabla} \times \{(f(r) \cdot \vec{r})\}$
- where
- $f(r)$
- is differentiable.
- (16  $\frac{2}{3}$ )

- (c) If
- $c_1$
- and
- $c_2$
- are constant vectors and
- $\lambda$
- is a constant scalar, show that
- $H = e^{-\lambda x} (c_1 \sin \lambda y + c_2 \cos \lambda y)$
- satisfies the partial differential equation
- $\frac{\partial^2 H}{\partial x^2} + \frac{\partial^2 H}{\partial y^2} = 0$
- .
- (15)

4. (a) If
- $\vec{F} = 4xi - 2y^2j + z^2k$
- and V is the volume of the cylinder
- $x^2 + y^2 = 4$
- ,
- $z = 0$
- and
- $z = 3$
- , evaluate
- $\iiint_V \vec{\nabla} \cdot \vec{F} dV$
- .
- (20)

- (b) State Stoke's theorem. Verify the theorem for
- $\vec{F} = (x+y)i + (2x-z)j + (y+z)k$
- taken over the triangle ABC cut off from the plane
- $3x+2y+z=6$
- by the coordinate planes.
- (26  $\frac{2}{3}$ )

**MATH 261 (ME)**

**SECTION – B**

There are **FOUR** questions in this section. Answer any **THREE**.

5. (a) By the method of Fröbenius, obtain two linearly independent solution valid about  $x = 0$  for the following differential equation: (36  $\frac{2}{3}$ )

$$2x^2 \frac{d^2 y}{dx^2} - x \frac{dy}{dx} + (1 - x^2)y = 0$$

- (b) Prove that  $J_n(x)$  and  $J_{-n}(x)$  are linearly dependent when  $n$  is any integer. (10)
6. (a) Show that  $\frac{d}{dx}[xJ_n(x)J_{n+1}(x)] = x[J_n^2(x) - J_{n+1}^2(x)]$ . (10)

- (b) Show that  $P_n(x)$  is the coefficient of  $z^n$  in the expansion of  $(1 - 2xz + z^2)^{-\frac{1}{2}}$  in ascending power of  $z$ . (20)

- (c) Show that  $p_n(x) = \frac{1}{\pi} \int_0^\pi [x \pm \sqrt{x^2 - 1} \cos \theta]^n d\theta$ , where  $n$  is a positive integer. (16  $\frac{2}{3}$ )

7. (a) Show that  $L\{\sin \sqrt{t}\} = \frac{\sqrt{\pi}}{2s^{3/2}} e^{-\frac{1}{4s}}$  and hence find  $L\left\{\frac{\cos \sqrt{t}}{\sqrt{t}}\right\}$ . (14)

- (b) Find (i)  $L^{-1}\left\{\frac{1}{(s^2 + a^2)^{3/2}}\right\}$  (10)

- (ii)  $L^{-1}\left\{\frac{s^2 + 2s + 3}{(s^2 + 2s + 2)(s^2 + 2s + 5)}\right\}$  (12)

- (c) Prove that  $\frac{1}{\pi} \int_0^\pi \cos(t \cos \theta) d\theta = J_0(t)$ . (10  $\frac{2}{3}$ )

8. (a) Using Laplace transformation, solve: (24)

$$\begin{aligned} x''(t) + y'(t) + 3x(t) &= 15e^{-t} \\ y''(t) - 4x'(t) + 3y(t) &= 15 \sin 2t \\ \text{with } x(0) = 35, \quad x'(0) &= -48 \\ y(0) = 27, \quad y'(0) &= -55 \end{aligned}$$

- (b) Solve the boundary value problem (using Laplace transformation): (22  $\frac{2}{3}$ )

$$\frac{\partial u}{\partial t} = 2 \frac{\partial^2 u}{\partial x^2}$$

with  $u(0, t) = 0$ ,  $u(5, t) = 0$  and  $u(x, 0) = 10 \sin 4\pi x - 5 \sin 6\pi x$

where,  $0 < x < 5$ ,  $t > 0$ .

BANGLADESH UNIVERSITY OF ENGINEERING AND TECHNOLOGY, DHAKA

L-2/T-1 B. Sc. Engineering Examinations 2015-2016

Sub : **ME 247** (Engineering Mechanics-I)

Full Marks: 210

Time : 3 Hours

USE SEPARATE SCRIPTS FOR EACH SECTION

The figures in the margin indicate full marks.

Symbols indicate their usual meaning. Assume any missing data.

**SECTION – A**There are **FOUR** questions in this section. Answer any **THREE**.

1. (a) Determine by direct integration, the centroid of the area shown in Fig. 1(a). Express your answer in terms of  $a$  and  $b$ . (17)  
 (b) A thin steel wire of uniform cross section is bent into the shape as shown in Fig. 1(b). Locate its center of gravity. (18)
  
2. (a) Two  $10^\circ$  wedges of negligible weight are used to move and position the 400-lb block. Knowing that the coefficient of static friction is 0.25 at all surfaces of contact, determine the smallest force  $P$  that should be applied to the wedge as shown in Fig. 2(a). (17)  
 (b) A 300-lb block is supported by a rope that is wrapped 1.5 times around a horizontal rod as shown in Fig. 2(b). Knowing that the coefficient of static friction between the rope and the rod is 0.15, determine the range of values of  $P$  for which equilibrium is maintained. (18)
  
3. (a) Determine the moments of inertia of the shaded area shown in Fig. 3(a) with respect to the  $x$  and  $y$  axes when  $a = 20$  mm. (17)  
 (b) A thin plate of mass  $m$  is cut in the shape of an equilateral triangle of side  $a$  as shown in Fig. 3(b). Determine the mass moment of inertia of the plate with respect to (i) the centroidal axes  $AA'$  and  $BB'$ , (ii) the centroidal axis  $CC'$  that is perpendicular to the plate. (18)
  
4. (a) Determine the vertical force  $P$  that must be applied at  $C$  to maintain the equilibrium of the linkage as shown in Fig. 4(a). Solve the problem using the principle of virtual work. (17)  
 (b) A cable is supporting three loads as shown in Fig. 4(b). Knowing that  $m_B = 18$  kg and  $m_C = 10$  kg, determine the magnitude of the force  $P$  required to maintain equilibrium. (18)

**SECTION – B**

There are **FOUR** questions in this section. Answer any **THREE**.

5. (a) A movable bin and its contents have a combined weight of 2.8 kN as shown in Fig. for Q. 5(a). Determine the shortest chain sling  $ACB$  that can be used to lift the loaded bin if the tension in the chain is not to exceed 5 kN. (17)

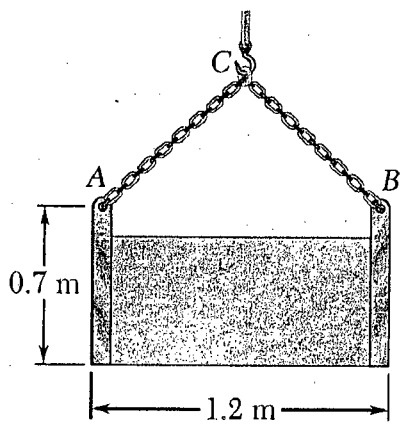


Fig. for Q.5(a)

- (b) Collars  $A$  and  $B$  are connected by a 525-mm-long wire and can slide freely on frictionless rods as shown in Fig. for Q. 5(b). If a force  $P = 341$  N is applied to collar  $A$ , determine (i) the tension in the wire when  $y = 155$  mm, (ii) the magnitude of the force  $Q$  required to maintain the equilibrium of the system. (18)

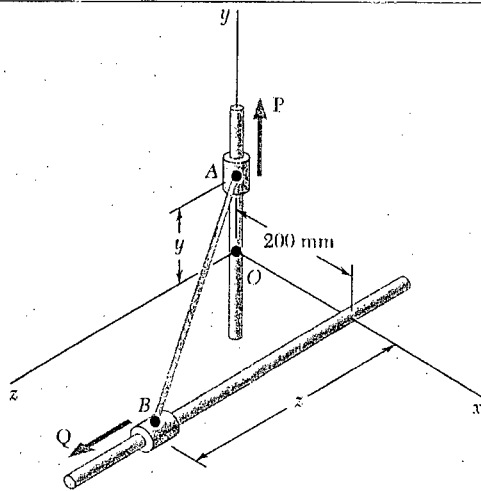


Fig. for Q.5(b)

6. (a) The frame  $ACD$  is hinged at  $A$  and  $D$  and is supported by a cable that passes through a ring at  $B$  and is attached to hooks at  $G$  and  $H$  as shown in Fig. for Q. 6(a). Knowing that the tension in the cable is 450 N, determine the moment about the diagonal  $AD$  of the force exerted on the frame by portion  $BH$  of the cable. (17)

- (b) Four forces act on a  $700 \times 375$ -mm plate as shown in Fig. for Q. 6(b). Locate the two points where the line of action of the resultant of these forces intersects the edge of the plate. (18)

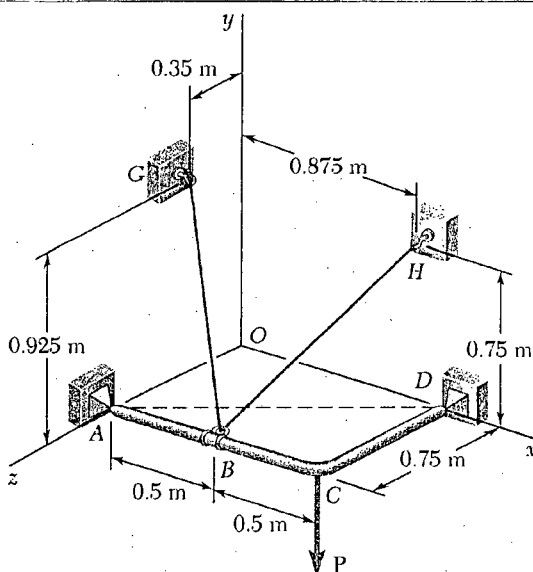


Fig. for Q.6(a)

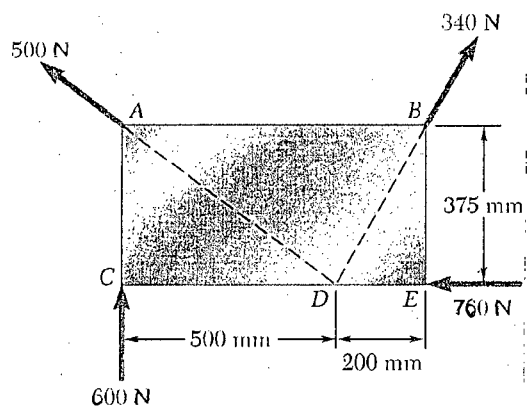
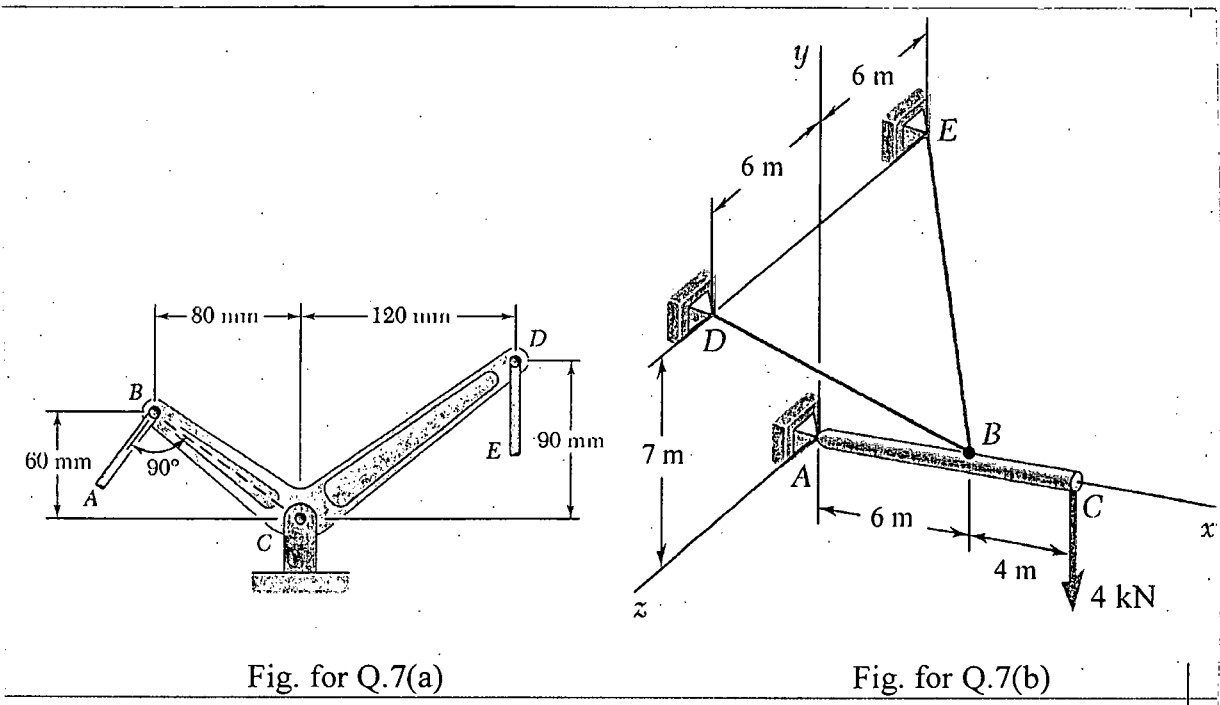


Fig. for Q.6(b)

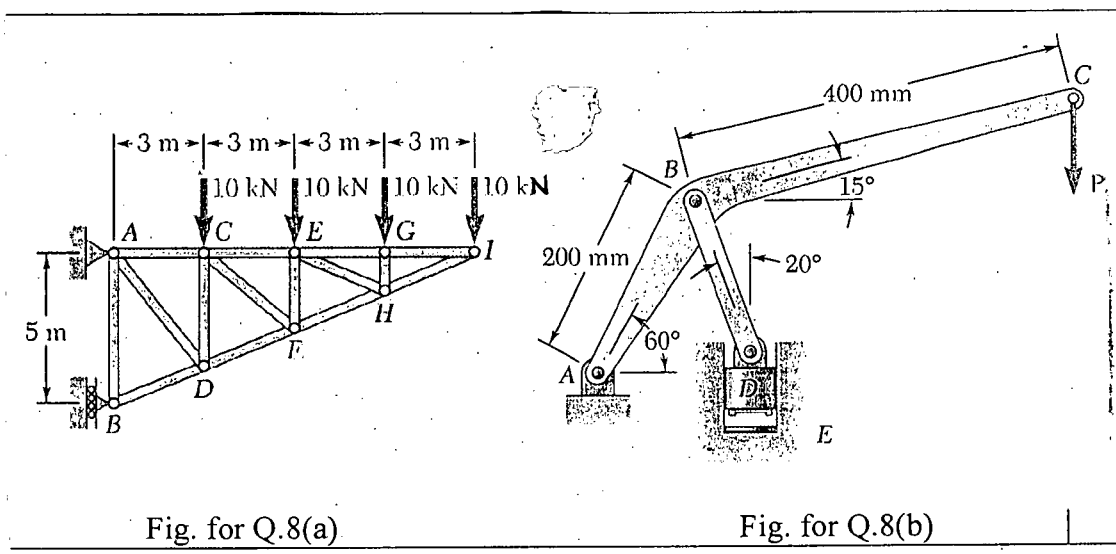
**ME 247/ME**

7. (a) Two links  $AB$  and  $DE$  are connected by a bell crank as shown in Fig. for Q. 7(a). Knowing that the tension in link  $AB$  is 720 N, determine (i) the tension in link  $DE$ , (ii) the reaction at  $C$ . (17)

- (b) A 10-m boom is acted upon by the 4-kN force as shown in Fig. for Q. 7(b). Determine the tension in each cable. (18)



8. (a) Determine the force in members  $CD$  and  $DF$  of the truss as shown in Fig. for Q. 8(a). (17)
- (b) The press as shown in Fig. for Q. 8(b) is used to emboss a small seal at  $E$ . Knowing that  $P = 250$  N, determine (i) the vertical component of the force exerted on the seal, (ii) the reaction at  $A$ . (18)



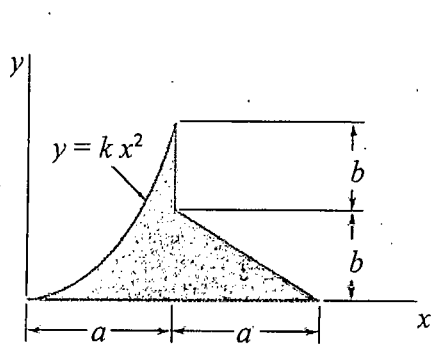


Fig. 1(a)

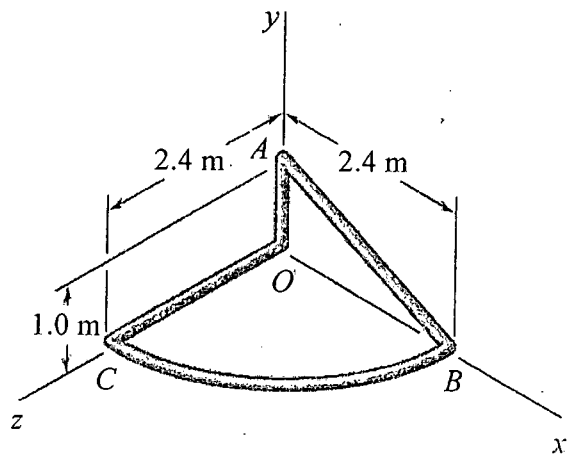


Fig. 1(b)

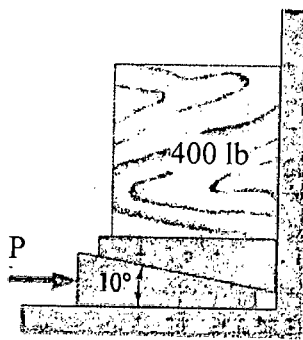


Fig. 2(a)

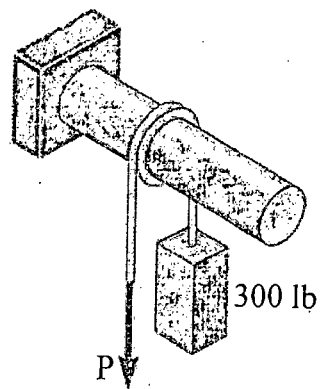


Fig. 2(b)

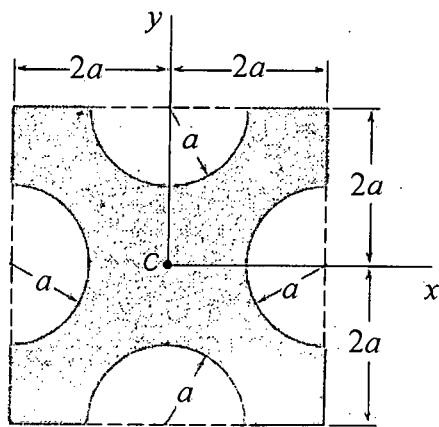


Fig. 3(a)

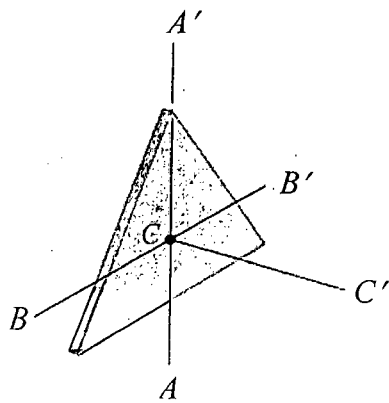


Fig. 3(b)

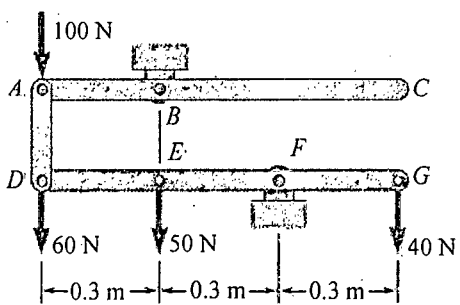


Fig. 4(a)

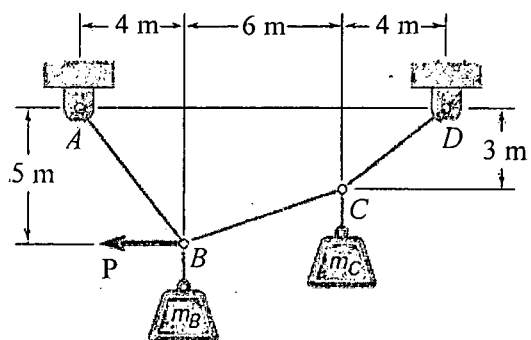


Fig. 4(b)

BANGLADESH UNIVERSITY OF ENGINEERING AND TECHNOLOGY, DHAKA

L-2/T-1 B. Sc. Engineering Examinations 2015-2016

Sub : **EEE 259** (Electrical and Electronic Technology)

Full Marks: 280

Time : 3 Hours

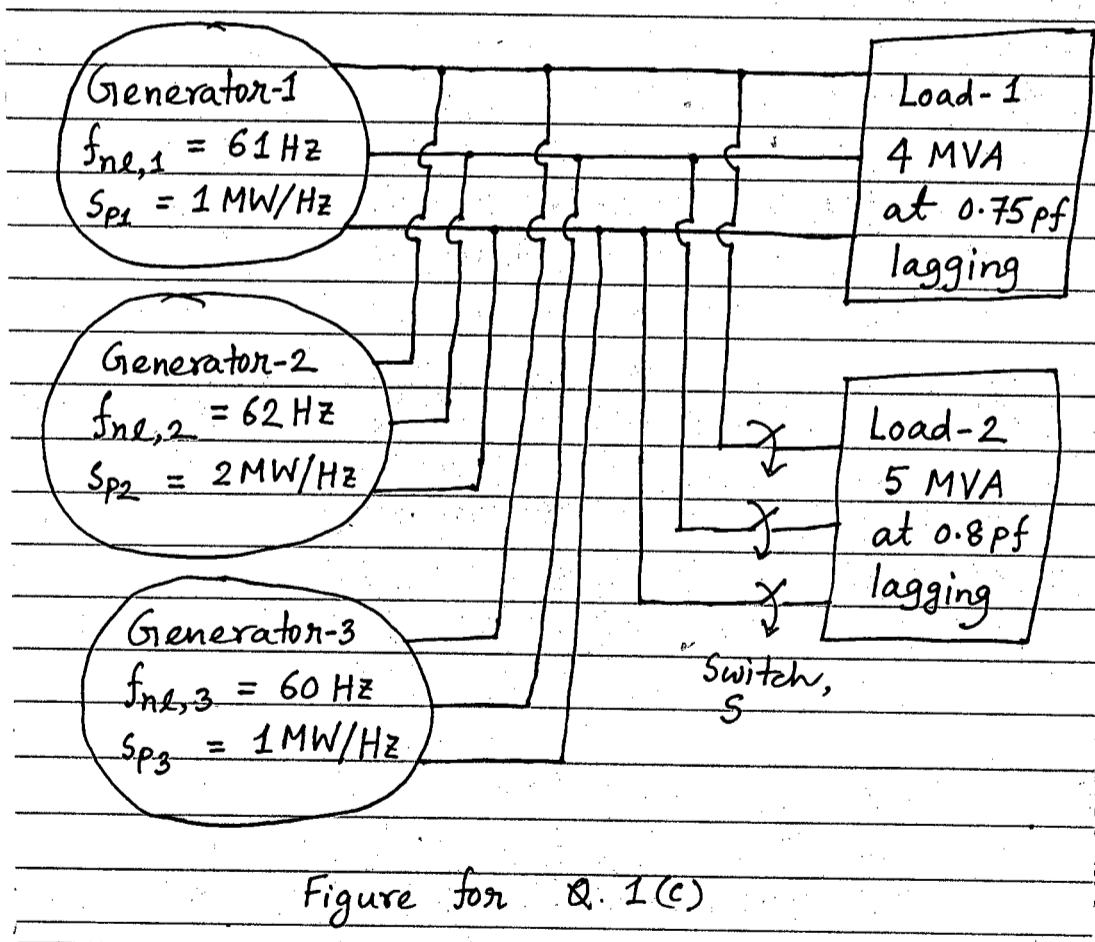
USE SEPARATE SCRIPTS FOR EACH SECTION

The figures in the margin indicate full marks.

**SECTION – A**There are **FOUR** questions in this section. Answer any **THREE**.

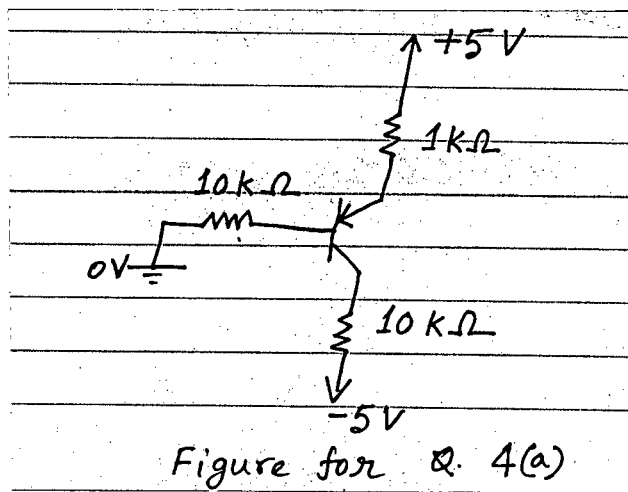
Symbols have their usual meaning.

1. (a) Mention 4 conditions required for paralleling synchronous generators. (8)
- (b) With necessary phasor diagrams, discuss the effect of load changes on a synchronous generator operating alone. (16 $\frac{2}{3}$ )
- (c) (i) Find operating frequency of the system shown in Figure for Q. 1(c) before closing switch S. Calculate power contribution of each generator. Is any generator working as a motor? (22)
- (ii) Find operating frequency, and power contribution of each generator after closing switch S.



**EEE 259/ME**

- 2. (a) Explain armature resistance speed control method of DC shunt motor. Why is this method less common? (13<sup>2</sup>/<sub>3</sub>)  
(b) Draw the equivalent circuit of a DC series motor. Also, derive the torque-speed characteristics equation of this motor. (13)  
(c) Draw and briefly explain a DC motor starting circuit using counter voltage-sensing relays to cut out the starting resistor. (20)
  
- 3. (a) With necessary diagrams, explain how total real power, total reactive power, and power factor of a balance 3-phase system can be measured from 2-wattmeter method experiment. (18)  
(b) With neat diagrams, explain the development and effects of armature reaction in a dc machine. (18)  
(c) Draw the power flow diagrams of DC motor and generator. (10<sup>2</sup>/<sub>3</sub>)
  
- 4. (a) Determine voltages at all nodes and currents through all branches for the circuit shown in Figure for Q. 4(a). Assume,  $\beta = 100$  for active mode. (16<sup>2</sup>/<sub>3</sub>)

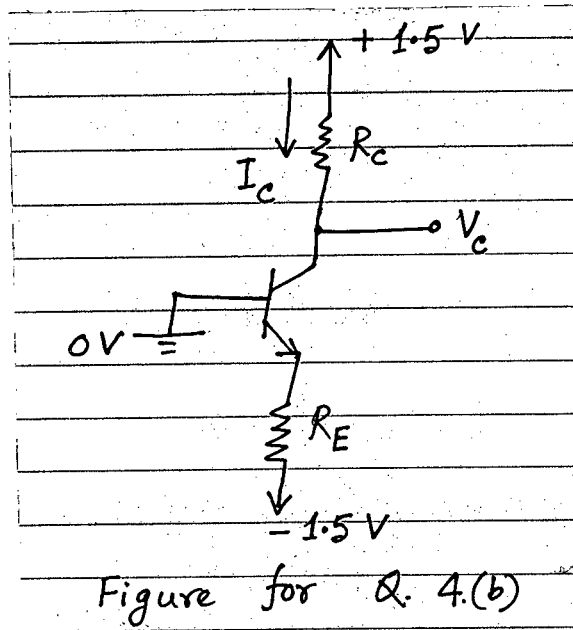




**EEE 259/ME**  
**Contd... Q. No. 4**

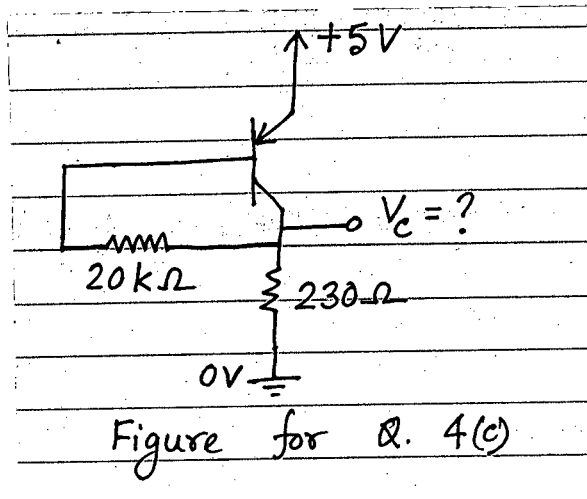
(b) Design the circuit shown in Figure for Q. 4(b) to establish  $I_C = 0.1 \text{ mA}$  and  $V_C = 0.5 \text{ V}$ . The transistor exhibits  $\beta = 100$ .

(15)



(c) Find collector voltage,  $V_C$  for the circuit shown in Figure for Q. 4(c). Assume,  $\beta = 100$ .

(15)



**SECTION - B**

There are **FOUR** questions in this section. Answer any **THREE**.

5. (a) Define Current Transformer (CT) and Potential Transformer (PT). (6<sup>2</sup>/<sub>3</sub>)
- (b) Derive the approximate equivalent circuit referred to primary of a transformer. (15)
- (c) A 20 kVA, 8000/480 V distribution transformer has the following per unit resistances and reactances: (25)

$R_{P,pu} = 0.01 \text{ p.u.}$	$R_{S,pu} = 0.0043 \text{ p.u.}$
$X_{P,pu} = 0.0141 \text{ p.u.}$	$X_{S,pu} = 0.0052 \text{ p.u.}$
$R_{C,pu} = 78.125 \text{ p.u.}$	$R_{M,pu} = 9.375 \text{ p.u.}$

**EEE 259/ME**

**Contd... Q. No. 5(c)**

The excitation branch impedances are given referred to high-voltage side.

- (i) Find the equivalent circuit of this transformer referred to high-voltage side.
- (ii) This transformer is supplying rated load at 480 V and 0.8 pF lagging. What is the transformer's input voltage? Determine the transformer's efficiency under this condition.

6. (a) A 20 kVA, 20,000/480-V, 50 Hz distribution transformer is tested with the following results: (26)

Open-circuit Test (measured from secondary side)	Short-circuit Test (measured from primary side)
$V_{OC} = 480 \text{ V}$	$V_{SC} = 1130 \text{ V}$
$I_{OC} = 1.60 \text{ A}$	$I_{SC} = 1.00 \text{ A}$
$P_{OC} = 305 \text{ W}$	$P_{SC} = 260 \text{ W}$

- (i) Find the equivalent circuit of this transformer referred to low-voltage side.
- (ii) Calculate the full load voltage regulation at 0.8 leading power factor.

(b) Define unit transformer. Why unit transformers are used? (6 2/3)

(c) Explain with example: "From a balanced three phase set of currents we can produce a constant amplitude rotating magnetic field". (14)

7. (a) Draw the power flow diagram of an induction motor. Show that induced torque of an induction motor is, (20 2/3)

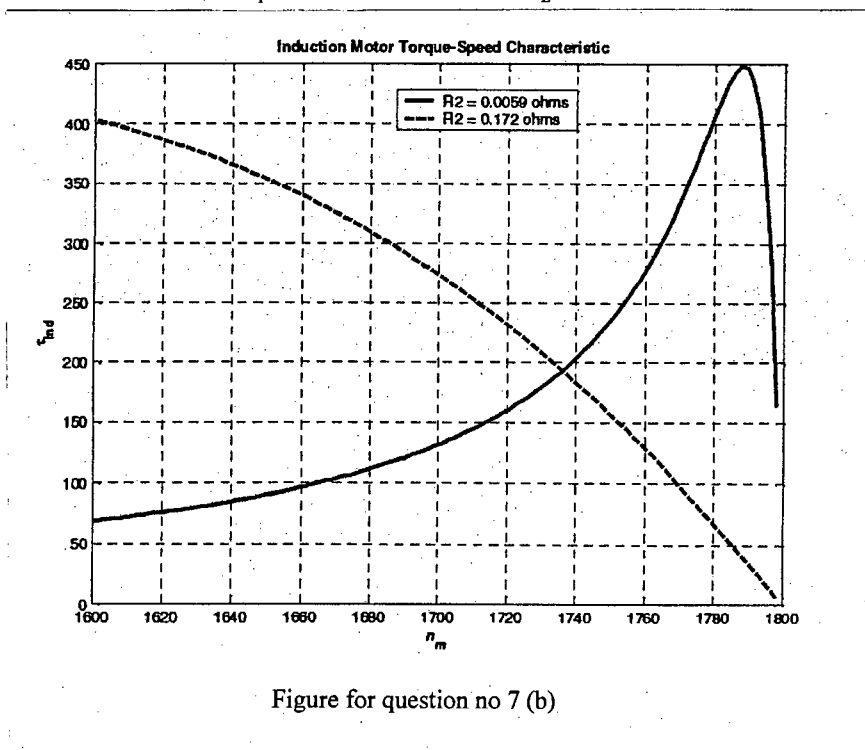
$$\tau_{ind} = \frac{P_{AG}}{\omega_{sync}}; \text{ where all symbols represent usual meanings}$$

(b) A 460-V, four pole, 50-hp, 60 Hz, Y-connected three-phase induction motor develops its full-load induced torque at 3.8% slip when operating at 60 Hz and 460 V.

The per-phase circuit model impedances of the motor are: (26)

$$R_1 = 0.33 \Omega \quad X_M = 30 \Omega$$

$$X_1 = 0.42 \Omega \quad X_2 = 0.42 \Omega$$



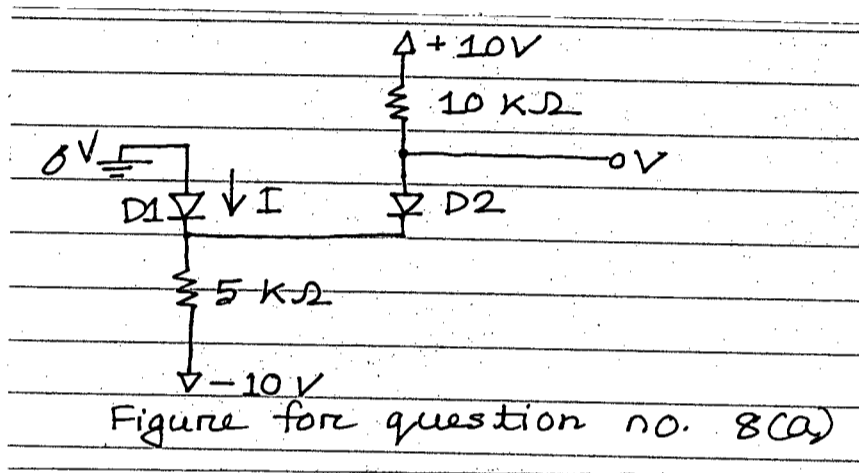
EEE 259/ME

Contd... Q. No. 7(b)

Neglect mechanical, core and stray losses for this problem.

- (i) Find the value of rotor resistance,  $R_F$  (use figure for question No. 7(b)).
- (ii) Find  $S_{max}$  and the rotor speed at maximum torque for this motor.
- (iii) Find starting torque of this motor.

8. (a) Find the values of  $I$  and  $V$  in the circuit shown in Figure for question No. 8(a).  
(Assume the diodes to be ideal) (17)



- (b) Assuming the diodes to be ideal, determine the transfer characteristics of the circuit shown in Figure for question No. 8(b). (17)

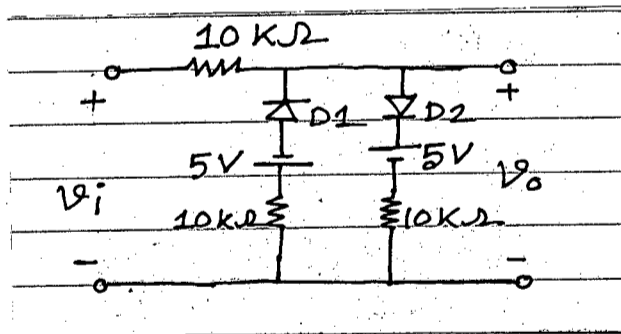


Figure for question no. 8(b)

- (c) Draw and explain a voltage doubler circuit. (12 $\frac{2}{3}$ )

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## BANGLADESH UNIVERSITY OF ENGINEERING AND TECHNOLOGY, DHAKA

L-2/T-1 B. Sc. Engineering Examinations 2015-2016

Sub : **HUM 303** (Principles of Accounting)

Full Marks: 210

Time : 3 Hours

USE SEPARATE SCRIPTS FOR EACH SECTION

The figures in the margin indicate full marks.

**SECTION – A**There are **FOUR** questions in this section. Answer any **THREE**.

1. (a) How is expense recognition principle connected with matching principle? Explain with example. (5)

- (b) Intesar Agency was opened at May 1, 2015. The following transactions occurred in the month of May— (20)

- May 1: Invested Tk. 500000 cash in the business.  
 May 2: Hired a employee at a monthly salary of Tk. 20000.  
 May 5: Paid advertising expense for the month in cash Tk. 5000.  
 May 6: Borrowed Tk. 50000 cash from a bank signing a note payable.  
 May 9: Service provided of Tk. 40000. 50% is on cash and remaining on account.  
 May 11: Purchase office equipment on account Tk. 30000.  
 May 14: Received Tk. 10000 cash from customers due on May 9.  
 May 25: Paid dues on equipment purchase.

**Required:**

- (i) Prepare a Journal Book for Intesar Agency for the month of May.  
 (ii) Prepare the ledger of 'Cash Account' and Service Revenue Account.  
 (c) What are the components of financial statements? What type of information is provided to the users through these components? Describe elaborately. (10)

2. (a) Anthony Gase has started his computer service business on April 1st of 2015. Following transactions occurred during the month. (16)

- April 1: Invested cash in the business Tk. 30,000.  
 April 2: Purchased computer terminals for Tk. 20,000 on account.  
 April 3: Purchase supplies for Tk. 1,500 cash.  
 April 6: Performed computer services Tk. 8,000 cash.  
 April 8: Paid dues for purchase on account on April 2.  
 April 19: Provide services on credit to customer Tk. 5000.  
 April 25: Paid expenses for the month: rent Tk. 10000; salaries Tk. 8000 and utilities bill Tk. 2000.  
 April 30: Received Tk. 5000 from the customer who was billed on April 19.

**Required:** Prepare a tabular summary for the month of April.

**HUM 303**

**Contd... Q. No. 2(a)**

(b) How do we differentiate revenue from gain and expense from loss? Illustrate your answer with examples. (7)

(c) Following information available for Zerox Product Company is presented below: (12)

	2014	2015
Net Sales (all in credit)	Tk. 720000	Tk. 750000
Cost of Goods Sold	440000	480000
Interest Expense	5000	7000
Net Income	42000	45000
Account Receivable	100000	120000
Inventory	75000	85000
Total Assets	500000	580000
Total Shareholders' Equity	325000	430000

**Required:**

- (i) Profit Margin.
- (ii) Asset turnover.
- (iii) Return on Assets.
- (iv) Return on Shareholders' Equity.
- (v) Inventory Turnover.
- (vi) Accounts Receivable turnover.

3. (a) Write down the two categories of adjusting entries and identify the type of adjustments applicable to each category. (8)

(b) The trial balance of "Wax Company" is given below— (27)

**Wax Company**  
Trial Balance  
December 31, 2015

Account Title	Debit (Tk.)	Credit (Tk.)
Cash	8000	
Accounts Receivable	4000	
Prepaid Insurance	2400	
Supplies	1500	
Office Equipment	12000	
Accounts Payable		3800
Unearned Service Revenue		3000
Salary expense	3000	
Rent expense	1900	
Capital		20000
Service revenue		6000
<b>Total</b>	<b>32800</b>	<b>32800</b>

**HUM 303**

**Contd... Q. No. 3(b)**

Other Information:

- Unused supplies on hand at December 31 were Tk. 500.
- Travel expense incurred but not paid Tk. 350.
- Insurance policy was for 2 years.
- Rent is accrued but not paid Tk. 900.
- Invoice represented that services earned for Tk. 1000 but not recorded.
- Office equipment is being depreciated at Tk. 250 per month.

**Required:**

- (i) Prepare necessary adjusting entries.
- (ii) Prepare an adjusted trial balance as at December 31, 2015.

4. (a) What is ratio analysis? Why is it important for business decision? (5)

(b) (30)

**Delta Company**  
Trial Balance  
31st December, 2015

Account Title	Debit (Tk.)	Credit (Tk.)
Accounts receivable	12000	
Accounts payable		6000
Cash	30500	
Trademark	20000	
Capital		50900
Supplies	900	
Salary expense	7000	
Sales person salary	3000	
Maintenance expense	4000	
Rent expense	13000	
Notes payable		5000
Bond payable		20000
Tax payable		20000
Store equipment	25000	
Machinery	2500	
Unearned commission		3000
Sales revenue		98000
Cost of goods sold	30000	
Prepaid insurance	4000	
Goodwill	51000	
<b>Total</b>	<b>20,2900</b>	<b>20,2900</b>

**HUM 303**

**Contd... Q. No. 4(b)**

Adjustment Data:

- (i) Two thirds of the supplies were used during the period.
- (ii) Charge @ 10% depreciation on store equipment.
- (iii) 60% rent relates to office and remaining to sales.

**Required:**

- (i) Prepare a multiple step (classified) income statement for the year ended December, 2015.
- (ii) Prepare an owner's equity statement.
- (iii) Prepare a classified balance sheet at 31st December, 2015.

**SECTION – B**

There are **FOUR** questions in this section. Answer any **THREE**.

5. (a) Write down the classification of manufacturing cost. (6)
- (b) Define the following cost concept with example: (6)
- (i) Opportunity cost.
  - (ii) Sunk cost.
  - (iii) Discretionary fixed cost.
- (c) The following cost and inventory data taken from the accounting records of Navana Company for the year ended on 31st December, 2014. (23)

Inventories	January 1, 2014	31 <sup>st</sup> December, 2014
Direct material	Tk. 7,000	Tk. 15,000
Work-in-process	10,000	5,000
Finished goods	20,000	35,000

Cost Incurred	Amount (Tk.)
Direct labor cost	70,000
Purchase of raw materials	118,500
Indirect labor	30,000
Maintenance, factory equipment	6,000
Advertising expense	90,000
Insurance, factory	800
Sales commission	35,000
Administrative managers salary	55,000
Supervisors salary	12,000

**HUM 303**

**Contd... Q. No. 5(c)**

Cost Incurred	Amount (Tk.)
Rent, factory	30,000
Rent, office	25,000
Rent for showroom	13,000
Utility (70% factory, 30% for office)	15,000
Supplies (60% factory, 40% for office)	3,000
Power and electricity	2,500
Fuel for factory equipment	700
Depreciation, factory equipment	30,000
Legal fees	15,000

**Required:**

(i) Prepare a cost of goods sold statement in a good form.

6. (a) What do you understand by cost structure? (5)

(b) Bogside farm and Steriling farm ae two blueberry farms. Bogside farm has higher variable cost as it depends on migrate workers to pick its berries by hand, whereas Sterling Farm has higher fixed cost as a result of its investment in expensive machine to pick its berries. Following are the income statements of these two blueberry farms: (10)

	Bogside farm	Sterling farm
Sales	Tk. 100,000	Tk. 100,000
Less: Variable expense	60,000	30,000
Contribution margin	40,000	70,000
Less: Fixed expense	30,000	60,000
Net profit	<b>10,000</b>	<b>10,000</b>

**Required:**

Considering CM ratio, break-even-point and margin of safety expression which farm has the better cost structure?

(c) Simens company manufactures and sells a specialized cordless telephone for the highest electromagnetic radiation environments. The company' contribution format income statement for recent year is given below: (20)

	Total (Tk.)	Per unit (Tk.)	Percentage(%)
Sales (20,000 units)	10,00,000	50	100
Less: Variable expense	<u>800,000</u>	<u>40</u>	<u>?</u>
Contribution margin	200,000	<u>10</u>	<u>?</u>
Less: Fixed cost	<u>150,000</u>		
Net profit	<b><u>50,000</u></b>		



**HUM 303**

**Contd... Q. No. 6(c)**

Management is anxious to increase company's profit and has asked for an analysis of a number of items.

**Required:**

- (i) Compute the company's CM ratio and variable expense ratio.
- (ii) Compute company's break-even-points in units and Tk.
- (iii) Assume that sales increase by Tk. 400,000 next year. If cost behavior patterns remain unchanged, by how much will the company's net operating income increase?
- (iv) Refer to the original data. Assume that next year management wants the company to earn a profit of at least Tk. 90,000. How many unit will have to be sold to meet this target profit?
- (v) Refer to the original data. Compute the company's margin of safety.

7. (a) In what situation, absorption costing will result higher net income than variable costing? Why? (5)

(b) For the income year ended on December 31, 2015; you have been given the information below: (18)

Selling price per unit	Tk. 50
<b><u>Manufacturing cost (Tk.)</u></b>	
Direct material cost per unit	8
Direct labor cost per unit	7
Variable manufacturing cost per unit	5
Fixed manufacturing cost for the period	Tk. 100,000
<b><u>Selling and administrative cost (Tk.)</u></b>	
Variable cost per unit	2
Fixed cost for the period	Tk. 80,000

During the year, a total 10,000 units produced but only 8,500 units sold.

**Required:**

- (i) Calculate the product cost per unit under absorption costing system and variable costing system.
  - (ii) Prepare income statement using under absorption costing system and variable costing system.
  - (iii) Reconcile the amount of profits under two costing systems.
- (c) "Singer Company" provides management consulting services to government and corporate clients. It has two supports departments- Finance (FIN) and Information technology (IT) – and two operating departments – Government Consulting (GOVT) and Corporate Consulting (CORP). For the year 2014, the following information was available: (12)

**HUM 303**

**Contd... Q. No. 7(c)**

Budgeted overhead before allocation	Support Dept.		Operating Dept.		Total
	FIN	IT	GOVT	CORP	
	60,000	24,000	80,000	120,000	
Support work by FIN	-	25%	40%	35%	100%
Support work by IT	10%	-	30%	60%	100%

**Required:** Allocate two supports departments cost to the two operating departments by using-

- (i) Direct method.
- (ii) Step-down method.

8. (a) Brentline Hospital is interested in predicting future monthly maintenance cost for budgeting purpose. The senior management team believes that maintenance is a mixed cost and that the variable portion of this cost is driven by the number of patient days. Each day a patient is in the hospital counts as one patient day. The Hospital's chief financial officer fathered the following data for the most recent seven months period:

(15)

Month	Activity level	Maintenance cost (Tk.)
January	5,600	7,900
February	7,100	8,500
March	5,000	7,400
April	6,500	8,200
May	7,300	9,100
June	8,000	9,800
July	6,200	7,800

**Required:**

- (i) Using high low method find out variable and fixed maintenance cost for the hospital.
  - (ii) Express the fixed and variable components of admitting cost as a cost formula in the form  $Y = a + bX$ .
  - (iii) Suppose in August the hospital is expecting that 5,500 patient will come. Now find out the budgeted variable cost, fixed cost and total cost for the month of August.
- (b) Write down the methods of mixed cost analysis.
- (c) What are the limitations of NPV (Net Present Value method)? Write with examples.

(5)

(3)

**HUM 303**

**Contd... Q. No. 8(c)**

(d) A company considering an investment proposal to install a new machine at a cost of Tk. 50,000. The estimated cash flows of the investment proposal are as follows:

**(12)**

Years	CFAT (Cash Flows Adjusted Time)
1	Tk. 10000
2	10450
3	11800
4	12250
5	16750

**Required:** Find out-

- (i) Pay Back Period.
  - (ii) IRR (Internal Rate of Return)
  - (iii) NPV (Net Present Value) at 10% cost of capital
  - (iv) PI (Profitability Index) @ discount rate is 10%.
-

BANGLADESH UNIVERSITY OF ENGINEERING AND TECHNOLOGY, DHAKA

L-2/T-1 B. Sc. Engineering Examinations 2015-2016

Sub : **ME 203** (Engineering Thermodynamics)

Full Marks: 210

Time : 3 Hours

USE SEPARATE SCRIPTS FOR EACH SECTION

The figures in the margin indicate full marks.

**SECTION – A**There are **FOUR** questions in this section. Answer any **THREE**.

Data tables are attached.

1. (a) Define 'work' and 'heat', and make brief comparison between them. (10)  
 (b) Briefly explain the general expression of work and write a short note on flow work. (10)  
 (c) A gas contained within a piston-cylinder device is initially at 1.0 MPa and 0.02 m<sup>3</sup>. It expands to a final volume of 0.04 m<sup>3</sup> under the conditions that (15)  
 (i) pressure remains constant  
 (ii) temperature remains constant.  
 Estimate heat transfer and work output.
2. (a) Briefly present First Law of thermodynamics for open system and derive Bernoulli's equation from it. (10)  
 (b) Mention some characteristics and origins of 'thermodynamic properties'. Show that, internal energy is a thermodynamic property. (10)  
 (c) A steam turbine operates with an initial condition of 30 bars and 400°C, 160 m/s and an outlet state of saturated vapour at 0.5 bar with a velocity of 100 m/s. The mass flow rate is 20 kg/s, and the power output is 10.8 MW. Estimate heat transfer neglecting friction. (15)
3. (a) Briefly present Clausius' statement of second law of thermodynamics. Show that, violation of this statement leads to violation of Kelvin-Planck statement. (10)  
 (b) Write a short note on 'Perpetual Motion Machine'. Show that, Kelvin-Planck statement states the impossibility of Perpetual Motion Machine of second kind. (10)  
 (c) Briefly explain the principle of increase of entropy. Apply this principle for the melting of ice at 25°C ambient condition. (15)
4. (a) Briefly explain (10)  
 (i) isentropic nozzle efficiency  
 (ii) isentropic turbine efficiency

**ME 203**

**Contd... Q. No. 4**

(b) Air is compressed isentropically from 100 kPa and 25°C to 500 kPa. Estimate the work required if the compressor is (10)

- (i) reciprocating type
- (ii) centrifugal type

(c) A turbine operating at steady state receives air at a pressure of  $P_1 = 3.0$  bar and temperature of  $T_1 = 400$  K. Air exits the turbine at  $P_2 = 1.0$  bar. Work developed is 74 kJ/kg of air. Using ideal gas model estimate isentropic turbine efficiency and entropy generation. (15)

**SECTION – B**

There are **FOUR** questions in this section. Answer any **THREE**.

Assume a reasonable value for any missing data.

Compressibility chart, R-134a properties table and steam table are provided.

5. (a) Determine the specific volume of refrigerant-134a at 1 MPa and 50°C, using: (i) the ideal gas equation of state and (ii) the generalized compressibility chart. (12)

(b) Refrigerant-134a enters the compressor of a refrigerator as superheated vapor at 0.14 MPa and  $-10^\circ\text{C}$  at a rate of 0.05 kg/s and leaves at 0.8 MPa and 50°C. The refrigerant is cooled in the condenser to 26°C and 0.72 MPa and is throttled to 0.15 MPa. Disregarding any heat transfer and pressure drops in the connecting lines between the components, determine: (23)

- (i) isentropic efficiency of the compressor
- (ii) COP of the refrigerator.

6. (a) An ideal gas-turbine cycle with two stages of compression and two stages of expansion has an overall pressure ratio of 8. Air enters each stage of the compressor at 300 K and each stage of the turbine at 1300 K. Determine the back work ratio and the thermal efficiency of this gas turbine cycle, assuming (i) no regenerators and (ii) an ideal regenerator with 100 percent effectiveness. (17 ½)

(b) An ideal diesel cycle with air as the working fluid has a compression ratio of 18 and a cut off ratio of 2. At the beginning of the compression process, the working fluid is at 100 kPa, 27°C, and 1917 cm<sup>3</sup>. Utilizing the cold-air-standard assumptions, determine: (17 ½)

- (i) Thermal efficiency of the cycle.
- (ii) Net work output of the cycle.
- (iii) The mean effective pressure.

**ME 203**

7. Consider a steam power plant operating on the ideal regenerative Rankine cycle with one open feed water heater. Steam enters the turbine at 15 MPa and 600°C and is condensed in the condenser at a pressure of 10 kPa. Some steam leaves the turbine at a pressure of 1.2 MPa and enters the open feed water heater. Isentropic efficiency of the turbine is 90%. Determine the fraction of steam extracted from the turbine and thermal efficiency of the cycle. (35)

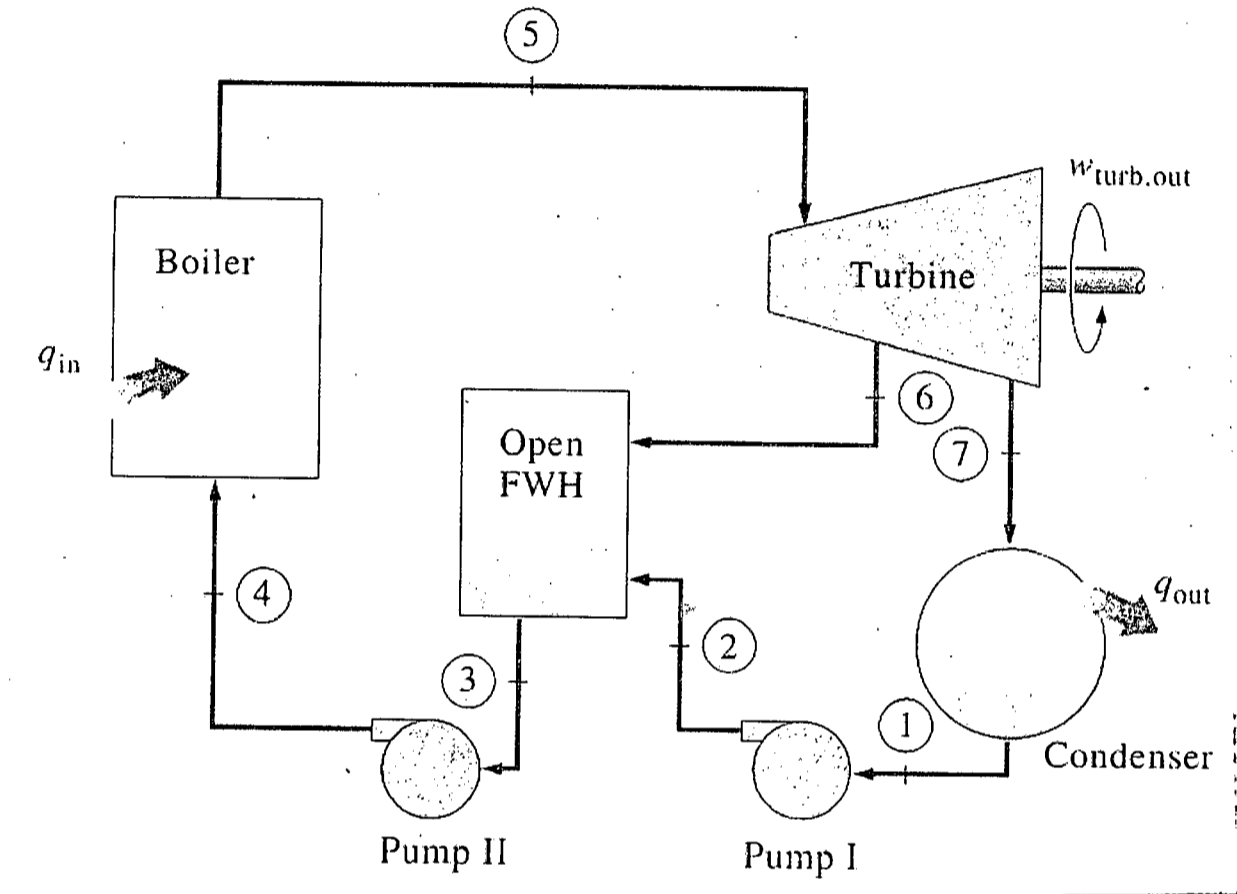


Fig. for Q. No. 7

8. (a) Make a brief comparison between 1 kJ of heat at 500°C and 1 kJ of heat at 2000°C. (5)
- (b) Prove that,  $\left(\frac{\partial u}{\partial v}\right)_T = T\left(\frac{\partial P}{\partial T}\right)_v - P$ . Using the expression, show that (10)
- (i)  $u = f(T)$ ; for ideal gas
- (ii)  $u = f(T, v)$  for Vander walls gas
- (c) A mixture consists of 10% O<sub>2</sub>, 70% N<sub>2</sub> and 10% CO<sub>2</sub> by mass. Determine: (10)
- (i) the molar analysis.
- (ii) the apparent gas constant.
- (d) Write short notes on: (10)
- (i) Joule-Thomson coefficient.
- (ii) Dew-point temperature.

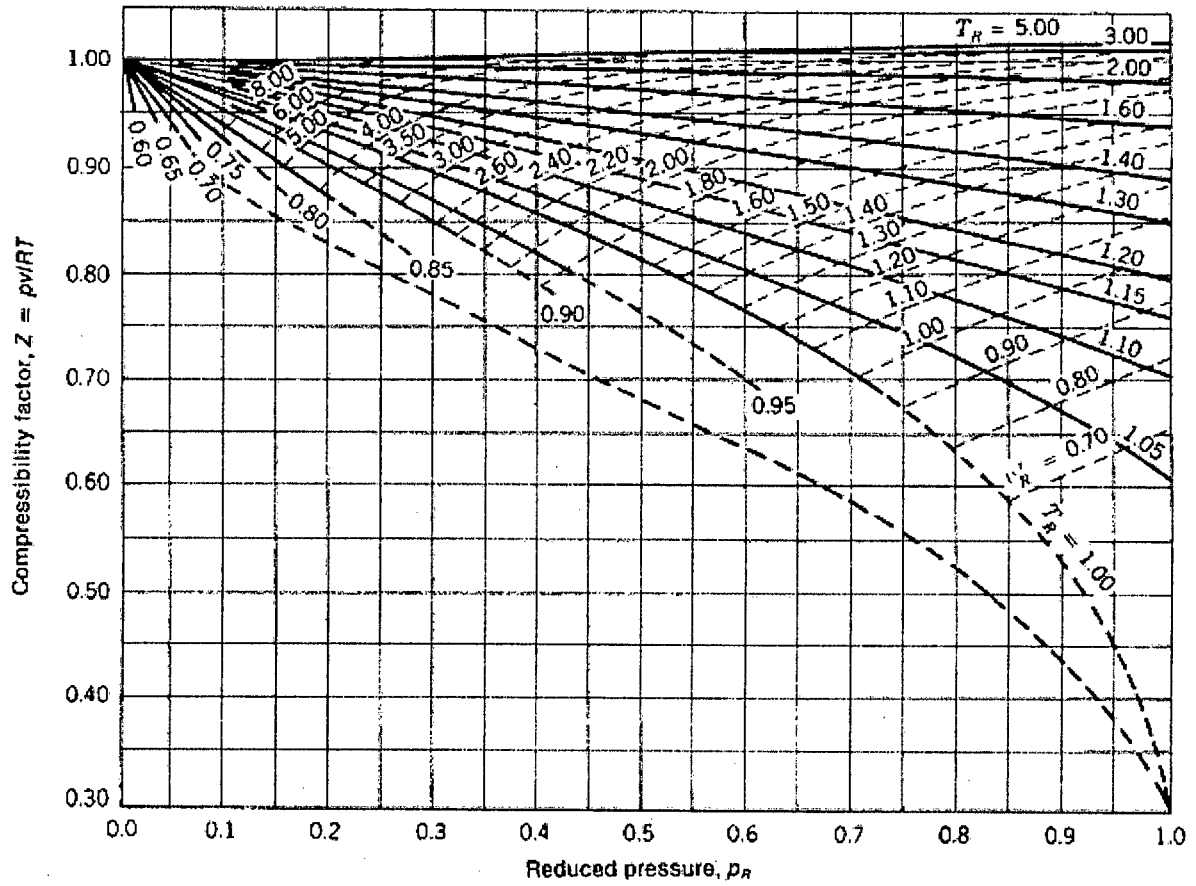


Figure A-1 Generalized compressibility chart,  $p_R \approx 1.0$ . Source: E. F. Obert, *Concepts of Thermodynamics*, McGraw-Hill, New York, 1960.

Tables in SI Units

TABLE A-10 Properties of Saturated Refrigerant 134a (Liquid-Vapor): Temperature Table

Temp. °C	Press. bar	Specific Volume m <sup>3</sup> /kg		Internal Energy kJ/kg		Enthalpy kJ/kg			Entropy kJ/kg · K		Temp. °C
		Sat. Liquid $v_f \times 10^3$	Sat. Vapor $v_g$	Sat. Liquid $u_f$	Sat. Vapor $u_g$	Sat. Liquid $h_f$	Evap. $h_{fg}$	Sat. Vapor $h_g$	Sat. Liquid $s_f$	Sat. Vapor $s_g$	
-40	0.5164	0.7055	0.3569	-0.04	204.45	0.00	222.88	222.88	0.0000	0.9560	-40
-36	0.6332	0.7113	0.2947	4.68	206.73	4.73	220.67	225.40	0.0201	0.9506	-36
-32	0.7704	0.7172	0.2451	9.47	209.01	9.52	218.37	227.90	0.0401	0.9456	-32
-28	0.9305	0.7233	0.2052	14.31	211.29	14.37	216.01	230.38	0.0600	0.9411	-28
-26	1.0199	0.7265	0.1882	16.75	212.43	16.82	214.80	231.62	0.0699	0.9390	-26
-24	1.1160	0.7296	0.1728	19.21	213.57	19.29	213.57	232.85	0.0798	0.9370	-24
-22	1.2192	0.7328	0.1590	21.68	214.70	21.77	212.32	234.08	0.0897	0.9351	-22
-20	1.3299	0.7361	0.1464	24.17	215.84	24.26	211.05	235.31	0.0996	0.9332	-20
-18	1.4483	0.7395	0.1350	26.67	216.97	26.77	209.76	236.53	0.1094	0.9315	-18
-16	1.5748	0.7428	0.1247	29.18	218.10	29.30	208.45	237.74	0.1192	0.9298	-16
-12	1.8540	0.7498	0.1068	34.25	220.36	34.39	205.77	240.15	0.1388	0.9267	-12
-8	2.1704	0.7569	0.0919	39.38	222.60	39.54	203.00	242.54	0.1583	0.9239	-8
-4	2.5274	0.7644	0.0794	44.56	224.84	44.75	200.15	244.90	0.1777	0.9213	-4
0	2.9282	0.7721	0.0689	49.79	227.06	50.02	197.21	247.23	0.1970	0.9190	0
4	3.3765	0.7801	0.0600	55.08	229.27	55.35	194.19	249.53	0.2162	0.9169	4
8	3.8756	0.7884	0.0525	60.43	231.46	60.73	191.07	251.80	0.2354	0.9150	8
12	4.4294	0.7971	0.0460	65.83	233.63	66.18	187.85	254.03	0.2545	0.9132	12
16	5.0416	0.8062	0.0405	71.29	235.78	71.69	184.52	256.22	0.2735	0.9116	16
20	5.7160	0.8157	0.0358	76.80	237.91	77.26	181.09	258.36	0.2924	0.9102	20
24	6.4566	0.8257	0.0317	82.37	240.01	82.90	177.55	260.45	0.3113	0.9089	24
26	6.8530	0.8309	0.0298	85.18	241.05	85.75	175.73	261.48	0.3208	0.9082	26
28	7.2675	0.8362	0.0281	88.00	242.08	88.61	173.89	262.50	0.3302	0.9076	28
30	7.7006	0.8417	0.0265	90.84	243.10	91.49	172.00	263.50	0.3396	0.9070	30
32	8.1528	0.8473	0.0250	93.70	244.12	94.39	170.09	264.48	0.3490	0.9064	32
34	8.6247	0.8530	0.0236	96.58	245.12	97.31	168.14	265.45	0.3584	0.9058	34
36	9.1168	0.8590	0.0223	99.47	246.11	100.25	166.15	266.40	0.3678	0.9053	36
38	9.6298	0.8651	0.0210	102.38	247.09	103.21	164.12	267.33	0.3772	0.9047	38
40	10.164	0.8714	0.0199	105.30	248.06	106.19	162.05	268.24	0.3866	0.9041	40
42	10.720	0.8780	0.0188	108.25	249.02	109.19	159.94	269.14	0.3960	0.9035	42
44	11.299	0.8847	0.0177	111.22	249.96	112.22	157.79	270.01	0.4054	0.9030	44
48	12.526	0.8989	0.0159	117.22	251.79	118.35	153.33	271.68	0.4243	0.9017	48
52	13.851	0.9142	0.0142	123.31	253.55	124.58	148.66	273.24	0.4432	0.9004	52
56	15.278	0.9308	0.0127	129.51	255.23	130.93	143.75	274.68	0.4622	0.8990	56
60	16.813	0.9488	0.0114	135.82	256.81	137.42	138.57	275.99	0.4814	0.8973	60
70	21.162	1.0027	0.0086	152.22	260.15	154.34	124.08	278.43	0.5302	0.8918	70
80	26.324	1.0766	0.0064	169.88	262.14	172.71	106.41	279.12	0.5814	0.8827	80
90	32.435	1.1949	0.0046	189.82	261.34	193.69	82.63	276.32	0.6380	0.8655	90
100	39.742	1.5443	0.0027	218.60	248.49	224.74	34.40	259.13	0.7196	0.8117	100

Source: Tables A-10 through A-12 are calculated based on equations from D. P. Wilson and R. S. Basu, "Thermodynamic Properties of a New Stratospherically Safe Working Fluid—Refrigerant 134a," *ASHRAE Trans.*, Vol. 94, Pt. 2, 1988, pp. 2095–2118.

R-134a



TABLE A-11 Properties of Saturated Refrigerant 134a (Liquid-Vapor): Pressure Table

Press. bar	Temp. °C	Specific Volume m <sup>3</sup> /kg		Internal Energy kJ/kg		Enthalpy kJ/kg			Entropy kJ/kg · K		Press. bar
		Sat. Liquid $v_f \times 10^3$	Sat. Vapor $v_g$	Sat. Liquid $u_f$	Sat. Vapor $u_g$	Sat. Liquid $h_f$	Evap. $h_{fg}$	Sat. Vapor $h_g$	Sat. Liquid $s_f$	Sat. Vapor $s_g$	
0.6	-37.07	0.7097	0.3100	3.41	206.12	3.46	221.27	224.72	0.0147	0.9520	0.6
0.8	-31.21	0.7184	0.2366	10.41	209.46	10.47	217.92	228.39	0.0440	0.9447	0.8
1.0	-26.43	0.7258	0.1917	16.22	212.18	16.29	215.06	231.35	0.0678	0.9395	1.0
1.2	-22.36	0.7323	0.1614	21.23	214.50	21.32	212.54	233.86	0.0879	0.9354	1.2
1.4	-18.80	0.7381	0.1395	25.66	216.52	25.77	210.27	236.04	0.1055	0.9322	1.4
1.6	-15.62	0.7435	0.1229	29.66	218.32	29.78	208.19	237.97	0.1211	0.9295	1.6
1.8	-12.73	0.7485	0.1098	33.31	219.94	33.45	206.26	239.71	0.1352	0.9273	1.8
2.0	-10.09	0.7532	0.0993	36.69	221.43	36.84	204.46	241.30	0.1481	0.9253	2.0
2.4	-5.37	0.7618	0.0834	42.77	224.07	42.95	201.14	244.09	0.1710	0.9222	2.4
2.8	-1.23	0.7697	0.0719	48.18	226.38	48.39	198.13	246.52	0.1911	0.9197	2.8
3.2	2.48	0.7770	0.0632	53.06	228.43	53.31	195.35	248.66	0.2089	0.9177	3.2
3.6	5.84	0.7839	0.0564	57.54	230.28	57.82	192.76	250.58	0.2251	0.9160	3.6
4.0	8.93	0.7904	0.0509	61.69	231.97	62.00	190.32	252.32	0.2399	0.9145	4.0
5.0	15.74	0.8056	0.0409	70.93	235.64	71.33	184.74	256.07	0.2723	0.9117	5.0
6.0	21.58	0.8196	0.0341	78.99	238.74	79.48	179.71	259.19	0.2999	0.9097	6.0
7.0	26.72	0.8328	0.0292	86.19	241.42	86.78	175.07	261.85	0.3242	0.9080	7.0
8.0	31.33	0.8454	0.0255	92.75	243.78	93.42	170.73	264.15	0.3459	0.9066	8.0
9.0	35.53	0.8576	0.0226	98.79	245.88	99.56	166.62	266.18	0.3656	0.9054	9.0
10.0	39.39	0.8695	0.0202	104.42	247.77	105.29	162.68	267.97	0.3838	0.9043	10.0
12.0	46.32	0.8928	0.0166	114.69	251.03	115.76	155.23	270.99	0.4164	0.9023	12.0
14.0	52.43	0.9159	0.0140	123.98	253.74	125.26	148.14	273.40	0.4453	0.9003	14.0
16.0	57.92	0.9392	0.0121	132.52	256.00	134.02	141.31	275.33	0.4714	0.8982	16.0
18.0	62.91	0.9631	0.0105	140.49	257.88	142.22	134.60	276.83	0.4954	0.8959	18.0
20.0	67.49	0.9878	0.0093	148.02	259.41	149.99	127.95	277.94	0.5178	0.8934	20.0
25.0	77.59	1.0562	0.0069	165.48	261.84	168.12	111.06	279.17	0.5687	0.8854	25.0
30.0	86.22	1.1416	0.0053	181.88	262.16	185.30	92.71	278.01	0.6156	0.8735	30.0

Tables in SI Units

TABLE A-12 Properties of Superheated Refrigerant 134a Vapor

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 0.6 \text{ bar} = 0.06 \text{ MPa}$ ( $T_{\text{sat}} = -37.07^\circ\text{C}$ )				$p = 1.0 \text{ bar} = 0.10 \text{ MPa}$ ( $T_{\text{sat}} = -26.43^\circ\text{C}$ )				
Sat.	0.31003	206.12	224.72	0.9520	0.19170	212.18	231.35	0.9395
-20	0.33536	217.86	237.98	1.0062	0.19770	216.77	236.54	0.9602
-10	0.34992	224.97	245.96	1.0371	0.20686	224.01	244.70	0.9918
0	0.36433	232.24	254.10	1.0675	0.21587	231.41	252.99	1.0227
10	0.37861	239.69	262.41	1.0973	0.22473	238.96	261.43	1.0531
20	0.39279	247.32	270.89	1.1267	0.23349	246.67	270.02	1.0829
30	0.40688	255.12	279.53	1.1557	0.24216	254.54	278.76	1.1122
40	0.42091	263.10	288.35	1.1844	0.25076	262.58	287.66	1.1411
50	0.43487	271.25	297.34	1.2126	0.25930	270.79	296.72	1.1696
60	0.44879	279.58	306.51	1.2405	0.26779	279.16	305.94	1.1977
70	0.46266	288.08	315.84	1.2681	0.27623	287.70	315.32	1.2254
80	0.47650	296.75	325.34	1.2954	0.28464	296.40	324.87	1.2528
90	0.49031	305.58	335.00	1.3224	0.29302	305.27	334.57	1.2799

$p = 1.4 \text{ bar} = 0.14 \text{ MPa}$ ( $T_{\text{sat}} = -18.80^\circ\text{C}$ )				$p = 1.8 \text{ bar} = 0.18 \text{ MPa}$ ( $T_{\text{sat}} = -12.73^\circ\text{C}$ )				
Sat.	0.13945	216.52	236.04	0.9322	0.10983	219.94	239.71	0.9273
-10	0.14549	223.03	243.40	0.9606	0.11135	222.02	242.06	0.9362
0	0.15219	230.55	251.86	0.9922	0.11678	229.67	250.69	0.9684
10	0.15875	238.21	260.43	1.0230	0.12207	237.44	259.41	0.9998
20	0.16520	246.01	269.13	1.0532	0.12723	245.33	268.23	1.0304
30	0.17155	253.96	277.97	1.0828	0.13230	253.36	277.17	1.0604
40	0.17783	262.06	286.96	1.1120	0.13730	261.53	286.24	1.0898
50	0.18404	270.32	296.09	1.1407	0.14222	269.85	295.45	1.1187
60	0.19020	278.74	305.37	1.1690	0.14710	278.31	304.79	1.1472
70	0.19633	287.32	314.80	1.1969	0.15193	286.93	314.28	1.1753
80	0.20241	296.06	324.39	1.2244	0.15672	295.71	323.92	1.2030
90	0.20846	304.95	334.14	1.2516	0.16148	304.63	333.70	1.2303
100	0.21449	314.01	344.04	1.2785	0.16622	313.72	343.63	1.2573

$p = 2.0 \text{ bar} = 0.20 \text{ MPa}$ ( $T_{\text{sat}} = -10.09^\circ\text{C}$ )				$p = 2.4 \text{ bar} = 0.24 \text{ MPa}$ ( $T_{\text{sat}} = -5.37^\circ\text{C}$ )				
Sat.	0.09933	221.43	241.30	0.9253	0.08343	224.07	244.09	0.9222
-10	0.09938	221.50	241.38	0.9256	0.08574	228.31	248.89	0.9399
0	0.10438	229.23	250.10	0.9582	0.08993	236.26	257.84	0.9721
10	0.10922	237.05	258.89	0.9898	0.09399	244.30	266.85	1.0034
20	0.11394	244.99	267.78	1.0206	0.09794	252.45	275.95	1.0339
30	0.11856	253.06	276.77	1.0508	0.10181	260.72	285.16	1.0637
40	0.12311	261.26	285.88	1.0804	0.10562	269.12	294.47	1.0930
50	0.12758	269.61	295.12	1.1094	0.10937	277.67	303.91	1.1218
60	0.13201	278.10	304.50	1.1380	0.11307	286.35	313.49	1.1501
70	0.13639	286.74	314.02	1.1661	0.11674	295.18	323.19	1.1780
80	0.14073	295.53	323.68	1.1939	0.12037	304.15	333.04	1.2055
90	0.14504	304.47	333.48	1.2212	0.12398	313.27	343.03	1.2326
100	0.14932	313.57	343.43	1.2483				

R-134a

TABLE A-12 (Continued)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 2.8 \text{ bar} = 0.28 \text{ MPa}$ ( $T_{\text{sat}} = -1.23^\circ\text{C}$ )				$p = 3.2 \text{ bar} = 0.32 \text{ MPa}$ ( $T_{\text{sat}} = 2.48^\circ\text{C}$ )				
Sat.	0.07193	226.38	246.52	0.9197	0.06322	228.43	248.66	0.9177
0	0.07240	227.37	247.64	0.9238				
10	0.07613	235.44	256.76	0.9566	0.06576	234.61	255.65	0.9427
20	0.07972	243.59	265.91	0.9883	0.06901	242.87	264.95	0.9749
30	0.08320	251.83	275.12	1.0192	0.07214	251.19	274.28	1.0062
40	0.08660	260.17	284.42	1.0494	0.07518	259.61	283.67	1.0367
50	0.08992	268.64	293.81	1.0789	0.07815	268.14	293.15	1.0665
60	0.09319	277.23	303.32	1.1079	0.08106	276.79	302.72	1.0957
70	0.09641	285.96	312.95	1.1364	0.08392	285.56	312.41	1.1243
80	0.09960	294.82	322.71	1.1644	0.08674	294.46	322.22	1.1525
90	0.10275	303.83	332.60	1.1920	0.08953	303.50	332.15	1.1802
100	0.10587	312.98	342.62	1.2193	0.09229	312.68	342.21	1.2076
110	0.10897	322.27	352.78	1.2461	0.09503	322.00	352.40	1.2345
120	0.11205	331.71	363.08	1.2727	0.09774	331.45	362.73	1.2611

$p = 4.0 \text{ bar} = 0.40 \text{ MPa}$ ( $T_{\text{sat}} = 8.93^\circ\text{C}$ )				
Sat.	0.05089	231.97	252.32	0.9145
10	0.05119	232.87	253.35	0.9182
20	0.05397	241.37	262.96	0.9515
30	0.05662	249.89	272.54	0.9837
40	0.05917	258.47	282.14	1.0148
50	0.06164	267.13	291.79	1.0452
60	0.06405	275.89	301.51	1.0748
70	0.06641	284.75	311.32	1.1038
80	0.06873	293.73	321.23	1.1322
90	0.07102	302.84	331.25	1.1602
100	0.07327	312.07	341.38	1.1878
110	0.07550	321.44	351.64	1.2149
120	0.07771	330.94	362.03	1.2417
130	0.07991	340.58	372.54	1.2681
140	0.08208	350.35	383.18	1.2941

$p = 5.0 \text{ bar} = 0.50 \text{ MPa}$ ( $T_{\text{sat}} = 15.74^\circ\text{C}$ )				
Sat.	0.04086	235.64	256.07	0.9117
10				
20	0.04188	239.40	260.34	0.9264
30	0.04416	248.20	270.28	0.9597
40	0.04633	256.99	280.16	0.9918
50	0.04842	265.83	290.04	1.0229
60	0.05043	274.73	299.95	1.0531
70	0.05240	283.72	309.92	1.0825
80	0.05432	292.80	319.96	1.1114
90	0.05620	302.00	330.10	1.1397
100	0.05805	311.31	340.33	1.1675
110	0.05988	320.74	350.68	1.1949
120	0.06168	330.30	361.14	1.2218
130	0.06347	339.98	371.72	1.2484
140	0.06524	349.79	382.42	1.2746

$p = 6.0 \text{ bar} = 0.60 \text{ MPa}$ ( $T_{\text{sat}} = 21.58^\circ\text{C}$ )				
Sat.	0.03408	238.74	259.19	0.9097
30	0.03581	246.41	267.89	0.9388
40	0.03774	255.45	278.09	0.9719
50	0.03958	264.48	288.23	1.0037
60	0.04134	273.54	298.35	1.0346
70	0.04304	282.66	308.48	1.0645
80	0.04469	291.86	318.67	1.0938
90	0.04631	301.14	328.93	1.1225
100	0.04790	310.53	339.27	1.1505
110	0.04946	320.03	349.70	1.1781
120	0.05099	329.64	360.24	1.2053
130	0.05251	339.38	370.88	1.2320
140	0.05402	349.23	381.64	1.2584
150	0.05550	359.21	392.52	1.2844
160	0.05698	369.32	403.51	1.3100

$p = 7.0 \text{ bar} = 0.70 \text{ MPa}$ ( $T_{\text{sat}} = 26.72^\circ\text{C}$ )				
Sat.	0.02918	241.42	261.85	0.9080
30	0.02979	244.51	265.37	0.9197
40	0.03157	253.83	275.93	0.9539
50	0.03324	263.08	286.35	0.9867
60	0.03482	272.31	296.69	1.0182
70	0.03634	281.57	307.01	1.0487
80	0.03781	290.88	317.35	1.0784
90	0.03924	300.27	327.74	1.1074
100	0.04064	309.74	338.19	1.1358
110	0.04201	319.31	348.71	1.1637
120	0.04335	328.98	359.33	1.1910
130	0.04468	338.76	370.04	1.2179
140	0.04599	348.66	380.86	1.2444
150	0.04729	358.68	391.79	1.2706
160	0.04857	368.82	402.82	1.2963

TABLE A-12 (Continued)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 8.0 \text{ bar} = 0.80 \text{ MPa}$ ( $T_{\text{sat}} = 31.33^\circ\text{C}$ )					$p = 9.0 \text{ bar} = 0.90 \text{ MPa}$ ( $T_{\text{sat}} = 35.53^\circ\text{C}$ )			
Sat.	0.02547	243.78	264.15	0.9066	0.02255	245.88	266.18	0.9054
40	0.02691	252.13	273.66	0.9374	0.02325	250.32	271.25	0.9217
50	0.02846	261.62	284.39	0.9711	0.02472	260.09	282.34	0.9566
60	0.02992	271.04	294.98	1.0034	0.02609	269.72	293.21	0.9897
70	0.03131	280.45	305.50	1.0345	0.02738	279.30	303.94	1.0214
80	0.03264	289.89	316.00	1.0647	0.02861	288.87	314.62	1.0521
90	0.03393	299.37	326.52	1.0940	0.02980	298.46	325.28	1.0819
100	0.03519	308.93	337.08	1.1227	0.03095	308.11	335.96	1.1109
110	0.03642	318.57	347.71	1.1508	0.03207	317.82	346.68	1.1392
120	0.03762	328.31	358.40	1.1784	0.03316	327.62	357.47	1.1670
130	0.03881	338.14	369.19	1.2055	0.03423	337.52	368.33	1.1943
140	0.03997	348.09	380.07	1.2321	0.03529	347.51	379.27	1.2211
150	0.04113	358.15	391.05	1.2584	0.03633	357.61	390.31	1.2475
160	0.04227	368.32	402.14	1.2843	0.03736	367.82	401.44	1.2735
170	0.04340	378.61	413.33	1.3098	0.03838	378.14	412.68	1.2992
180	0.04452	389.02	424.63	1.3351	0.03939	388.57	424.02	1.3245
$p = 10.0 \text{ bar} = 1.00 \text{ MPa}$ ( $T_{\text{sat}} = 39.39^\circ\text{C}$ )					$p = 12.0 \text{ bar} = 1.20 \text{ MPa}$ ( $T_{\text{sat}} = 46.32^\circ\text{C}$ )			
Sat.	0.02020	247.77	267.97	0.9043	0.01663	251.03	270.99	0.9023
40	0.02029	248.39	268.68	0.9066	0.01712	254.98	275.52	0.9164
50	0.02171	258.48	280.19	0.9428	0.01835	265.42	287.44	0.9527
60	0.02301	268.35	291.36	0.9768	0.01947	275.59	298.96	0.9868
70	0.02423	278.11	302.34	1.0093	0.02051	285.62	310.24	1.0192
80	0.02538	287.82	313.20	1.0405	0.02150	295.59	321.39	1.0503
90	0.02649	297.53	324.01	1.0707	0.02244	305.54	332.47	1.0804
100	0.02755	307.27	334.82	1.1000	0.02335	315.50	343.52	1.1096
110	0.02858	317.06	345.65	1.1286	0.02423	325.51	354.58	1.1381
120	0.02959	326.93	356.52	1.1567	0.02508	335.58	365.68	1.1660
130	0.03058	336.88	367.46	1.1841	0.02592	345.73	376.83	1.1933
140	0.03154	346.92	378.46	1.2111	0.02674	355.95	388.04	1.2201
150	0.03250	357.06	389.56	1.2376	0.02754	366.27	399.33	1.2465
160	0.03344	367.31	400.74	1.2638	0.02834	376.69	410.70	1.2724
170	0.03436	377.66	412.02	1.2895	0.02912	387.21	422.16	1.2980
180	0.03528	388.12	423.40	1.3149				
$p = 14.0 \text{ bar} = 1.40 \text{ MPa}$ ( $T_{\text{sat}} = 52.43^\circ\text{C}$ )					$p = 16.0 \text{ bar} = 1.60 \text{ MPa}$ ( $T_{\text{sat}} = 57.92^\circ\text{C}$ )			
Sat.	0.01405	253.74	273.40	0.9003	0.01208	256.00	275.33	0.8982
60	0.01495	262.17	283.10	0.9297	0.01233	258.48	278.20	0.9069
70	0.01603	272.87	295.31	0.9658	0.01340	269.89	291.33	0.9457
80	0.01701	283.29	307.10	0.9997	0.01435	280.78	303.74	0.9813
90	0.01792	293.55	318.63	1.0319	0.01521	291.39	315.72	1.0148
100	0.01878	303.73	330.02	1.0628	0.01601	301.84	327.46	1.0467
110	0.01960	313.88	341.32	1.0927	0.01677	312.20	339.04	1.0773
120	0.02039	324.05	352.59	1.1218	0.01750	322.53	350.53	1.1069
130	0.02115	334.25	363.86	1.1501	0.01820	332.87	361.99	1.1357
140	0.02189	344.50	375.15	1.1777	0.01887	343.24	373.44	1.1638
150	0.02262	354.82	386.49	1.2048	0.01953	353.66	384.91	1.1912
160	0.02333	365.22	397.89	1.2315	0.02017	364.15	396.43	1.2181
170	0.02403	375.71	409.36	1.2576	0.02080	374.71	407.99	1.2445
180	0.02472	386.29	420.90	1.2834	0.02142	385.35	419.62	1.2704
190	0.02541	396.96	432.53	1.3088	0.02203	396.08	431.33	1.2960
200	0.02608	407.73	444.24	1.3338	0.02263	406.90	443.11	1.3212

R-134a

Tables in SI Units

TABLE A-2 Properties of Saturated Water (Liquid-Vapor): Temperature Table

H<sub>2</sub>O

Temp. °C	Press. bar	Specific Volume m <sup>3</sup> /kg		Internal Energy kJ/kg		Enthalpy kJ/kg			Entropy kJ/kg · K		Temp. °C
		Sat. Liquid $v_f \times 10^3$	Sat. Vapor $v_g$	Sat. Liquid $u_f$	Sat. Vapor $u_g$	Sat. Liquid $h_f$	Evap. $h_{fg}$	Sat. Vapor $h_g$	Sat. Liquid $s_f$	Sat. Vapor $s_g$	
.01	0.00611	1.0002	206.136	0.00	2375.3	0.01	2501.3	2501.4	0.0000	9.1562	.01
4	0.00813	1.0001	157.232	16.77	2380.9	16.78	2491.9	2508.7	0.0610	9.0514	4
5	0.00872	1.0001	147.120	20.97	2382.3	20.98	2489.6	2510.6	0.0761	9.0257	5
6	0.00935	1.0001	137.734	25.19	2383.6	25.20	2487.2	2512.4	0.0912	9.0003	6
8	0.01072	1.0002	120.917	33.59	2386.4	33.60	2482.5	2516.1	0.1212	8.9501	8
10	0.01228	1.0004	106.379	42.00	2389.2	42.01	2477.7	2519.8	0.1510	8.9008	10
11	0.01312	1.0004	99.857	46.20	2390.5	46.20	2475.4	2521.6	0.1658	8.8765	11
12	0.01402	1.0005	93.784	50.41	2391.9	50.41	2473.0	2523.4	0.1806	8.8524	12
13	0.01497	1.0007	88.124	54.60	2393.3	54.60	2470.7	2525.3	0.1953	8.8285	13
14	0.01598	1.0008	82.848	58.79	2394.7	58.80	2468.3	2527.1	0.2099	8.8048	14
15	0.01705	1.0009	77.926	62.99	2396.1	62.99	2465.9	2528.9	0.2245	8.7814	15
16	0.01818	1.0011	73.333	67.18	2397.4	67.19	2463.6	2530.8	0.2390	8.7582	16
17	0.01938	1.0012	69.044	71.38	2398.8	71.38	2461.2	2532.6	0.2535	8.7351	17
18	0.02064	1.0014	65.038	75.57	2400.2	75.58	2458.8	2534.4	0.2679	8.7123	18
19	0.02198	1.0016	61.293	79.76	2401.6	79.77	2456.5	2536.2	0.2823	8.6897	19
20	0.02339	1.0018	57.791	83.95	2402.9	83.96	2454.1	2538.1	0.2966	8.6672	20
21	0.02487	1.0020	54.514	88.14	2404.3	88.14	2451.8	2539.9	0.3109	8.6450	21
22	0.02645	1.0022	51.447	92.32	2405.7	92.33	2449.4	2541.7	0.3251	8.6229	22
23	0.02810	1.0024	48.574	96.51	2407.0	96.52	2447.0	2543.5	0.3393	8.6011	23
24	0.02985	1.0027	45.883	100.70	2408.4	100.70	2444.7	2545.4	0.3534	8.5794	24
25	0.03169	1.0029	43.360	104.88	2409.8	104.89	2442.3	2547.2	0.3674	8.5580	25
26	0.03363	1.0032	40.994	109.06	2411.1	109.07	2439.9	2549.0	0.3814	8.5367	26
27	0.03567	1.0035	38.774	113.25	2412.5	113.25	2437.6	2550.8	0.3954	8.5156	27
28	0.03782	1.0037	36.690	117.42	2413.9	117.43	2435.2	2552.6	0.4093	8.4946	28
29	0.04008	1.0040	34.733	121.60	2415.2	121.61	2432.8	2554.5	0.4231	8.4739	29
30	0.04246	1.0043	32.894	125.78	2416.6	125.79	2430.5	2556.3	0.4369	8.4533	30
31	0.04496	1.0046	31.165	129.96	2418.0	129.97	2428.1	2558.1	0.4507	8.4329	31
32	0.04759	1.0050	29.540	134.14	2419.3	134.15	2425.7	2559.9	0.4644	8.4127	32
33	0.05034	1.0053	28.011	138.32	2420.7	138.33	2423.4	2561.7	0.4781	8.3927	33
34	0.05324	1.0056	26.571	142.50	2422.0	142.50	2421.0	2563.5	0.4917	8.3728	34
35	0.05628	1.0060	25.216	146.67	2423.4	146.68	2418.6	2565.3	0.5053	8.3531	35
36	0.05947	1.0063	23.940	150.85	2424.7	150.86	2416.2	2567.1	0.5188	8.3336	36
38	0.06632	1.0071	21.602	159.20	2427.4	159.21	2411.5	2570.7	0.5458	8.2950	38
40	0.07384	1.0078	19.523	167.56	2430.1	167.57	2406.7	2574.3	0.5725	8.2570	40
45	0.09593	1.0099	15.258	188.44	2436.8	188.45	2394.8	2583.2	0.6387	8.1648	45

TABLE A-2 (Continued)

Temp. °C	Press. bar	Specific Volume m <sup>3</sup> /kg		Internal Energy kJ/kg		Enthalpy kJ/kg			Entropy kJ/kg · K		Temp. °C
		Sat. Liquid $v_f \times 10^3$	Sat. Vapor $v_g$	Sat. Liquid $u_f$	Sat. Vapor $u_g$	Sat. Liquid $h_f$	Evap. $h_{fg}$	Sat. Vapor $h_g$	Sat. Liquid $s_f$	Sat. Vapor $s_g$	
50	.1235	1.0121	12.032	209.32	2443.5	209.33	2382.7	2592.1	.7038	8.0763	50
55	.1576	1.0146	9.568	230.21	2450.1	230.23	2370.7	2600.9	.7679	7.9913	55
60	.1994	1.0172	7.671	251.11	2456.6	251.13	2358.5	2609.6	.8312	7.9096	60
65	.2503	1.0199	6.197	272.02	2463.1	272.06	2346.2	2618.3	.8935	7.8310	65
70	.3119	1.0228	5.042	292.95	2469.6	292.98	2333.8	2626.8	.9549	7.7553	70
75	.3858	1.0259	4.131	313.90	2475.9	313.93	2321.4	2635.3	1.0155	7.6824	75
80	.4739	1.0291	3.407	334.86	2482.2	334.91	2308.8	2643.7	1.0753	7.6122	80
85	.5783	1.0325	2.828	355.84	2488.4	355.90	2296.0	2651.9	1.1343	7.5445	85
90	.7014	1.0360	2.361	376.85	2494.5	376.92	2283.2	2660.1	1.1925	7.4791	90
95	.8455	1.0397	1.982	397.88	2500.6	397.96	2270.2	2668.1	1.2500	7.4159	95
100	1.014	1.0435	1.673	418.94	2506.5	419.04	2257.0	2676.1	1.3069	7.3549	100
110	1.433	1.0516	1.210	461.14	2518.1	461.30	2230.2	2691.5	1.4185	7.2387	110
120	1.985	1.0603	0.8919	503.50	2529.3	503.71	2202.6	2706.3	1.5276	7.1296	120
130	2.701	1.0697	0.6685	546.02	2539.9	546.31	2174.2	2720.5	1.6344	7.0269	130
140	3.613	1.0797	0.5089	588.74	2550.0	589.13	2144.7	2733.9	1.7391	6.9299	140
150	4.758	1.0905	0.3928	631.68	2559.5	632.20	2114.3	2746.5	1.8418	6.8379	150
160	6.178	1.1020	0.3071	674.86	2568.4	675.55	2082.6	2758.1	1.9427	6.7502	160
170	7.917	1.1143	0.2428	718.33	2576.5	719.21	2049.5	2768.7	2.0419	6.6663	170
180	10.02	1.1274	0.1941	762.09	2583.7	763.22	2015.0	2778.2	2.1396	6.5857	180
190	12.54	1.1414	0.1565	806.19	2590.0	807.62	1978.8	2786.4	2.2359	6.5079	190
200	15.54	1.1565	0.1274	850.65	2595.3	852.45	1940.7	2793.2	2.3309	6.4323	200
210	19.06	1.1726	0.1044	895.53	2599.5	897.76	1900.7	2798.5	2.4248	6.3585	210
220	23.18	1.1900	0.08619	940.87	2602.4	943.62	1858.5	2802.1	2.5178	6.2861	220
230	27.95	1.2088	0.07158	986.74	2603.9	990.12	1813.8	2804.0	2.6099	6.2146	230
240	33.44	1.2291	0.05976	1033.2	2604.0	1037.3	1766.5	2803.8	2.7015	6.1437	240
250	39.73	1.2512	0.05013	1080.4	2602.4	1085.4	1716.2	2801.5	2.7927	6.0730	250
260	46.88	1.2755	0.04221	1128.4	2599.0	1134.4	1662.5	2796.6	2.8838	6.0019	260
270	54.99	1.3023	0.03564	1177.4	2593.7	1184.5	1605.2	2789.7	2.9751	5.9301	270
280	64.12	1.3321	0.03017	1227.5	2586.1	1236.0	1543.6	2779.6	3.0668	5.8571	280
290	74.36	1.3656	0.02557	1278.9	2576.0	1289.1	1477.1	2766.2	3.1594	5.7821	290
300	85.81	1.4036	0.02167	1332.0	2563.0	1344.0	1404.9	2749.0	3.2534	5.7045	300
320	112.7	1.4988	0.01549	1444.6	2525.5	1461.5	1238.6	2700.1	3.4480	5.5362	320
340	145.9	1.6379	0.01080	1570.3	2464.6	1594.2	1027.9	2622.0	3.6594	5.3357	340
360	186.5	1.8925	0.006945	1725.2	2351.5	1760.5	720.5	2481.0	3.9147	5.0526	360
374.14	220.9	3.155	0.003155	2029.6	2029.6	2099.3	0	2099.3	4.4298	4.4298	374.14

Source: Tables A-2 through A-5 are extracted from J. H. Keenan, F. G. Keyes, P. G. Hill, and J. G. Moore, *Steam Tables*, Wiley, New York, 1969.

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## Tables in SI Units

TABLE A-3 Properties of Saturated Water (Liquid-Vapor): Pressure Table

Press. bar	Temp. °C	Specific Volume m <sup>3</sup> /kg		Internal Energy kJ/kg		Enthalpy kJ/kg			Entropy kJ/kg · K		Press. bar
		Sat. Liquid $v_f \times 10^3$	Sat. Vapor $v_g$	Sat. Liquid $u_f$	Sat. Vapor $u_g$	Sat. Liquid $h_f$	Evap. $h_{fg}$	Sat. Vapor $h_g$	Sat. Liquid $s_f$	Sat. Vapor $s_g$	
0.04	28.96	1.0040	34.800	121.45	2415.2	121.46	2432.9	2554.4	0.4226	8.4746	0.04
0.06	36.16	1.0064	23.739	151.53	2425.0	151.53	2415.9	2567.4	0.5210	8.3304	0.06
0.08	41.51	1.0084	18.103	173.87	2432.2	173.88	2403.1	2577.0	0.5926	8.2287	0.08
0.10	45.81	1.0102	14.674	191.82	2437.9	191.83	2392.8	2584.7	0.6493	8.1502	0.10
0.20	60.06	1.0172	7.649	251.38	2456.7	251.40	2358.3	2609.7	0.8320	7.9085	0.20
0.30	69.10	1.0223	5.229	289.20	2468.4	289.23	2336.1	2625.3	0.9439	7.7686	0.30
0.40	75.87	1.0265	3.993	317.53	2477.0	317.58	2319.2	2636.8	1.0259	7.6700	0.40
0.50	81.33	1.0300	3.240	340.44	2483.9	340.49	2305.4	2645.9	1.0910	7.5939	0.50
0.60	85.94	1.0331	2.732	359.79	2489.6	359.86	2293.6	2653.5	1.1453	7.5320	0.60
0.70	89.95	1.0360	2.365	376.63	2494.5	376.70	2283.3	2660.0	1.1919	7.4797	0.70
0.80	93.50	1.0380	2.087	391.58	2498.8	391.66	2274.1	2665.8	1.2329	7.4346	0.80
0.90	96.71	1.0410	1.869	405.06	2502.6	405.15	2265.7	2670.9	1.2695	7.3949	0.90
1.00	99.63	1.0432	1.694	417.36	2506.1	417.46	2258.0	2675.5	1.3026	7.3594	1.00
1.50	111.4	1.0528	1.159	466.94	2519.7	467.11	2226.5	2693.6	1.4336	7.2233	1.50
2.00	120.2	1.0605	0.8857	504.49	2529.5	504.70	2201.9	2706.7	1.5301	7.1271	2.00
2.50	127.4	1.0672	0.7187	535.10	2537.2	535.37	2181.5	2716.9	1.6072	7.0527	2.50
3.00	133.6	1.0732	0.6058	561.15	2543.6	561.47	2163.8	2725.3	1.6718	6.9919	3.00
3.50	138.9	1.0786	0.5243	583.95	2546.9	584.33	2148.1	2732.4	1.7275	6.9405	3.50
4.00	143.6	1.0836	0.4625	604.31	2553.6	604.74	2133.8	2738.6	1.7766	6.8959	4.00
4.50	147.9	1.0882	0.4140	622.25	2557.6	623.25	2120.7	2743.9	1.8207	6.8565	4.50
5.00	151.9	1.0926	0.3749	639.68	2561.2	640.23	2108.5	2748.7	1.8607	6.8212	5.00
6.00	158.9	1.1006	0.3157	669.90	2567.4	670.56	2086.3	2756.8	1.9312	6.7600	6.00
7.00	165.0	1.1080	0.2729	696.44	2572.5	697.22	2066.3	2763.5	1.9922	6.7080	7.00
8.00	170.4	1.1148	0.2404	720.22	2576.8	721.11	2048.0	2769.1	2.0462	6.6628	8.00
9.00	175.4	1.1212	0.2150	741.83	2580.5	742.83	2031.1	2773.9	2.0946	6.6226	9.00
10.0	179.9	1.1273	0.1944	761.68	2583.6	762.81	2015.3	2778.1	2.1387	6.5863	10.0
15.0	198.3	1.1539	0.1318	843.16	2594.5	844.84	1947.3	2792.2	2.3150	6.4448	15.0
20.0	212.4	1.1767	0.09963	906.44	2600.3	908.79	1890.7	2799.5	2.4474	6.3409	20.0
25.0	224.0	1.1973	0.07998	959.11	2603.1	962.11	1841.0	2803.1	2.5547	6.2575	25.0
30.0	233.9	1.2165	0.06668	1004.8	2604.1	1008.4	1795.7	2804.2	2.6457	6.1869	30.0
35.0	242.6	1.2347	0.05707	1045.4	2603.7	1049.8	1753.7	2803.4	2.7253	6.1253	35.0
40.0	250.4	1.2522	0.04978	1082.3	2602.3	1087.3	1714.1	2801.4	2.7964	6.0701	40.0
45.0	257.5	1.2692	0.04406	1116.2	2600.1	1121.9	1676.4	2798.3	2.8610	6.0199	45.0
50.0	264.0	1.2859	0.03944	1147.8	2597.1	1154.2	1640.1	2794.3	2.9202	5.9734	50.0
60.0	275.6	1.3187	0.03244	1205.4	2589.7	1213.4	1571.0	2784.3	3.0267	5.8892	60.0
70.0	285.9	1.3513	0.02737	1257.6	2580.5	1267.0	1505.1	2772.1	3.1211	5.8133	70.0
80.0	295.1	1.3842	0.02352	1305.6	2569.8	1316.6	1441.3	2758.0	3.2068	5.7432	80.0
90.0	303.4	1.4178	0.02048	1350.5	2557.8	1363.3	1378.9	2742.1	3.2858	5.6772	90.0
100.	311.1	1.4524	0.01803	1393.0	2544.4	1407.6	1317.1	2724.7	3.3596	5.6141	100.
110.	318.2	1.4886	0.01599	1433.7	2529.8	1450.1	1255.5	2705.6	3.4295	5.5527	110.

H<sub>2</sub>O

TABLE A-3 (Continued)

Press. bar	Temp. °C	Specific Volume m <sup>3</sup> /kg		Internal Energy kJ/kg		Enthalpy kJ/kg			Entropy kJ/kg · K		Press. bar
		Sat. Liquid $v_f \times 10^3$	Sat. Vapor $v_g$	Sat. Liquid $u_f$	Sat. Vapor $u_g$	Sat. Liquid $h_f$	Evap. $h_{fg}$	Sat. Vapor $h_g$	Sat. Liquid $s_f$	Sat. Vapor $s_g$	
120.	324.8	1.5267	0.01426	1473.0	2513.7	1491.3	1193.6	2684.9	3.4962	5.4924	120.
130.	330.9	1.5671	0.01278	1511.1	2496.1	1531.5	1130.7	2662.2	3.5606	5.4323	130.
140.	336.8	1.6107	0.01149	1548.6	2476.8	1571.1	1066.5	2637.6	3.6232	5.3717	140.
150.	342.2	1.6581	0.01034	1585.6	2455.5	1610.5	1000.0	2610.5	3.6848	5.3098	150.
160.	347.4	1.7107	0.009306	1622.7	2431.7	1650.1	930.6	2580.6	3.7461	5.2455	160.
170.	352.4	1.7702	0.008364	1660.2	2405.0	1690.3	856.9	2547.2	3.8079	5.1777	170.
180.	357.1	1.8397	0.007489	1698.9	2374.3	1732.0	777.1	2509.1	3.8715	5.1044	180.
190.	361.5	1.9243	0.006657	1739.9	2338.1	1776.5	688.0	2464.5	3.9388	5.0228	190.
200.	365.8	2.036	0.005834	1785.6	2293.0	1826.3	583.4	2409.7	4.0139	4.9269	200.
220.9	374.1	3.155	0.003155	2029.6	2029.6	2099.3	0	2099.3	4.4298	4.4298	220.9

H<sub>2</sub>O



Tables in SI Units

TABLE A-4 Properties of Superheated Water Vapor

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 0.06 \text{ bar} = 0.006 \text{ MPa}$ ( $T_{\text{sat}} = 36.16^\circ\text{C}$ )					$p = 0.35 \text{ bar} = 0.035 \text{ MPa}$ ( $T_{\text{sat}} = 72.69^\circ\text{C}$ )			
Sat.	23.739	2425.0	2567.4	8.3304	4.526	2473.0	2631.4	7.7158
80	27.132	2487.3	2650.1	8.5804	4.625	2483.7	2645.6	7.7564
120	30.219	2544.7	2726.0	8.7840	5.163	2542.4	2723.1	7.9644
160	33.302	2602.7	2802.5	8.9693	5.696	2601.2	2800.6	8.1519
200	36.383	2661.4	2879.7	9.1398	6.228	2660.4	2878.4	8.3237
240	39.462	2721.0	2957.8	9.2982	6.758	2720.3	2956.8	8.4828
280	42.540	2781.5	3036.8	9.4464	7.287	2780.9	3036.0	8.6314
320	45.618	2843.0	3116.7	9.5859	7.815	2842.5	3116.1	8.7712
360	48.696	2905.5	3197.7	9.7180	8.344	2905.1	3197.1	8.9034
400	51.774	2969.0	3279.6	9.8435	8.872	2968.6	3279.2	9.0291
440	54.851	3033.5	3362.6	9.9633	9.400	3033.2	3362.2	9.1490
500	59.467	3132.3	3489.1	10.1336	10.192	3132.1	3488.8	9.3194
$p = 0.70 \text{ bar} = 0.07 \text{ MPa}$ ( $T_{\text{sat}} = 89.95^\circ\text{C}$ )					$p = 1.0 \text{ bar} = 0.10 \text{ MPa}$ ( $T_{\text{sat}} = 99.63^\circ\text{C}$ )			
Sat.	2.365	2494.5	2660.0	7.4797	1.694	2506.1	2675.5	7.3594
100	2.434	2509.7	2680.0	7.5341	1.696	2506.7	2676.2	7.3614
120	2.571	2539.7	2719.6	7.6375	1.793	2537.3	2716.6	7.4668
160	2.841	2599.4	2798.2	7.8279	1.984	2597.8	2796.2	7.6597
200	3.108	2659.1	2876.7	8.0012	2.172	2658.1	2875.3	7.8343
240	3.374	2719.3	2955.5	8.1611	2.359	2718.5	2954.5	7.9949
280	3.640	2780.2	3035.0	8.3162	2.546	2779.6	3034.2	8.1445
320	3.905	2842.0	3115.3	8.4504	2.732	2841.5	3114.6	8.2849
360	4.170	2904.6	3196.5	8.5828	2.917	2904.2	3195.9	8.4175
400	4.434	2968.2	3278.6	8.7086	3.103	2967.9	3278.2	8.5435
440	4.698	3032.9	3361.8	8.8286	3.288	3032.6	3361.4	8.6636
500	5.095	3131.8	3488.5	8.9991	3.565	3131.6	3488.1	8.8342
$p = 1.5 \text{ bar} = 0.15 \text{ MPa}$ ( $T_{\text{sat}} = 111.37^\circ\text{C}$ )					$p = 3.0 \text{ bar} = 0.30 \text{ MPa}$ ( $T_{\text{sat}} = 133.55^\circ\text{C}$ )			
Sat.	1.159	2519.7	2693.6	7.2233	0.606	2543.6	2725.3	6.9919
120	1.188	2533.3	2711.4	7.2693	0.651	2587.1	2782.3	7.1276
160	1.317	2595.2	2792.8	7.4665	0.716	2650.7	2865.5	7.3115
200	1.444	2656.2	2872.9	7.6433	0.781	2713.1	2947.3	7.4774
240	1.570	2717.2	2952.7	7.8052	0.844	2775.4	3028.6	7.6299
280	1.695	2778.6	3032.8	7.9555	0.907	2838.1	3110.1	7.7722
320	1.819	2840.6	3113.5	8.0964	0.969	2901.4	3192.2	7.9061
360	1.943	2903.5	3195.0	8.2293	1.032	2965.6	3275.0	8.0330
400	2.067	2967.3	3277.4	8.3555	1.094	3030.6	3358.7	8.1538
440	2.191	3032.1	3360.7	8.4757	1.187	3130.0	3486.0	8.3251
500	2.376	3131.2	3487.6	8.6466	1.341	3300.8	3703.2	8.5892
600	2.685	3301.7	3704.3	8.9101				

H<sub>2</sub>O

TABLE A-4 (Continued)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 5.0 \text{ bar} = 0.50 \text{ MPa}$ ( $T_{\text{sat}} = 151.86^\circ\text{C}$ )				$p = 7.0 \text{ bar} = 0.70 \text{ MPa}$ ( $T_{\text{sat}} = 164.97^\circ\text{C}$ )				
Sat.	0.3749	2561.2	2748.7	6.8213	0.2729	2572.5	2763.5	6.7080
180	0.4045	2609.7	2812.0	6.9656	0.2847	2599.8	2799.1	6.7880
200	0.4249	2642.9	2855.4	7.0592	0.2999	2634.8	2844.8	6.8865
240	0.4646	2707.6	2939.9	7.2307	0.3292	2701.8	2932.2	7.0641
280	0.5034	2771.2	3022.9	7.3865	0.3574	2766.9	3017.1	7.2233
320	0.5416	2834.7	3105.6	7.5308	0.3852	2831.3	3100.9	7.3697
360	0.5796	2898.7	3188.4	7.6660	0.4126	2895.8	3184.7	7.5063
400	0.6173	2963.2	3271.9	7.7938	0.4397	2960.9	3268.7	7.6350
440	0.6548	3028.6	3356.0	7.9152	0.4667	3026.6	3353.3	7.7571
500	0.7109	3128.4	3483.9	8.0873	0.5070	3126.8	3481.7	7.9299
600	0.8041	3299.6	3701.7	8.3522	0.5738	3298.5	3700.2	8.1956
700	0.8969	3477.5	3925.9	8.5952	0.6403	3476.6	3924.8	8.4391
$p = 10.0 \text{ bar} = 1.0 \text{ MPa}$ ( $T_{\text{sat}} = 179.91^\circ\text{C}$ )				$p = 15.0 \text{ bar} = 1.5 \text{ MPa}$ ( $T_{\text{sat}} = 198.32^\circ\text{C}$ )				
Sat.	0.1944	2583.6	2778.1	6.5865	0.1318	2594.5	2792.2	6.4448
200	0.2060	2621.9	2827.9	6.6940	0.1325	2598.1	2796.8	6.4546
240	0.2275	2692.9	2920.4	6.8817	0.1483	2676.9	2899.3	6.6628
280	0.2480	2760.2	3008.2	7.0465	0.1627	2748.6	2992.7	6.8381
320	0.2678	2826.1	3093.9	7.1962	0.1765	2817.1	3081.9	6.9938
360	0.2873	2891.6	3178.9	7.3349	0.1899	2884.4	3169.2	7.1363
400	0.3066	2957.3	3263.9	7.4651	0.2030	2951.3	3255.8	7.2690
440	0.3257	3023.6	3349.3	7.5883	0.2160	3018.5	3342.5	7.3940
500	0.3541	3124.4	3478.5	7.7622	0.2352	3120.3	3473.1	7.5698
540	0.3729	3192.6	3565.6	7.8720	0.2478	3189.1	3560.9	7.6805
600	0.4011	3296.8	3697.9	8.0290	0.2668	3293.9	3694.0	7.8385
640	0.4198	3367.4	3787.2	8.1290	0.2793	3364.8	3783.8	7.9391
$p = 20.0 \text{ bar} = 2.0 \text{ MPa}$ ( $T_{\text{sat}} = 212.42^\circ\text{C}$ )				$p = 30.0 \text{ bar} = 3.0 \text{ MPa}$ ( $T_{\text{sat}} = 233.90^\circ\text{C}$ )				
Sat.	0.0996	2600.3	2799.5	6.3409	0.0667	2604.1	2804.2	6.1869
240	0.1085	2659.6	2876.5	6.4952	0.0682	2619.7	2824.3	6.2265
280	0.1200	2736.4	2976.4	6.6828	0.0771	2709.9	2941.3	6.4462
320	0.1308	2807.9	3069.5	6.8452	0.0850	2788.4	3043.4	6.6245
360	0.1411	2877.0	3159.3	6.9917	0.0923	2861.7	3138.7	6.7801
400	0.1512	2945.2	3247.6	7.1271	0.0994	2932.8	3230.9	6.9212
440	0.1611	3013.4	3335.5	7.2540	0.1062	3002.9	3321.5	7.0520
500	0.1757	3116.2	3467.6	7.4317	0.1162	3108.0	3456.5	7.2338
540	0.1853	3185.6	3556.1	7.5434	0.1227	3178.4	3546.6	7.3474
600	0.1996	3290.9	3690.1	7.7024	0.1324	3285.0	3682.3	7.5085
640	0.2091	3362.2	3780.4	7.8035	0.1388	3357.0	3773.5	7.6106
700	0.2232	3470.9	3917.4	7.9487	0.1484	3466.5	3911.7	7.7571

Tables in SI Units

TABLE A-4 (Continued)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 40 \text{ bar} = 4.0 \text{ MPa}$ ( $T_{\text{sat}} = 250.4^\circ\text{C}$ )					$p = 60 \text{ bar} = 6.0 \text{ MPa}$ ( $T_{\text{sat}} = 275.64^\circ\text{C}$ )			
Sat.	0.04978	2602.3	2801.4	6.0701	0.03244	2589.7	2784.3	5.8892
280	0.05546	2680.0	2901.8	6.2568	0.03317	2605.2	2804.2	5.9252
320	0.06199	2767.4	3015.4	6.4553	0.03876	2720.0	2952.6	6.1846
360	0.06788	2845.7	3117.2	6.6215	0.04331	2811.2	3071.1	6.3782
400	0.07341	2919.9	3213.6	6.7690	0.04739	2892.9	3177.2	6.5408
440	0.07872	2992.2	3307.1	6.9041	0.05122	2970.0	3277.3	6.6853
500	0.08643	3099.5	3445.3	7.0901	0.05665	3082.2	3422.2	6.8803
540	0.09145	3171.1	3536.9	7.2056	0.06015	3156.1	3517.0	6.9999
600	0.09885	3279.1	3674.4	7.3688	0.06525	3266.9	3658.4	7.1677
640	0.1037	3351.8	3766.6	7.4720	0.06859	3341.0	3752.6	7.2731
700	0.1110	3462.1	3905.9	7.6198	0.07352	3453.1	3894.1	7.4234
740	0.1157	3536.6	3999.6	7.7141	0.07677	3528.3	3989.2	7.5190
$p = 80 \text{ bar} = 8.0 \text{ MPa}$ ( $T_{\text{sat}} = 295.06^\circ\text{C}$ )					$p = 100 \text{ bar} = 10.0 \text{ MPa}$ ( $T_{\text{sat}} = 311.06^\circ\text{C}$ )			
Sat.	0.02352	2569.8	2758.0	5.7432	0.01803	2544.4	2724.7	5.6141
320	0.02682	2662.7	2877.2	5.9489	0.01925	2588.8	2781.3	5.7103
360	0.03089	2772.7	3019.8	6.1819	0.02331	2729.1	2962.1	6.0060
400	0.03432	2863.8	3138.3	6.3634	0.02641	2832.4	3096.5	6.2120
440	0.03742	2946.7	3246.1	6.5190	0.02911	2922.1	3213.2	6.3805
480	0.04034	3025.7	3348.4	6.6586	0.03160	3005.4	3321.4	6.5282
520	0.04313	3102.7	3447.7	6.7871	0.03394	3085.6	3425.1	-6.6622
560	0.04582	3178.7	3545.3	6.9072	0.03619	3164.1	3526.0	6.7864
600	0.04845	3254.4	3642.0	7.0206	0.03837	3241.7	3625.3	6.9029
640	0.05102	3330.1	3738.3	7.1283	0.04048	3318.9	3723.7	7.0131
700	0.05481	3443.9	3882.4	7.2812	0.04358	3434.7	3870.5	7.1687
740	0.05729	3520.4	3978.7	7.3782	0.04560	3512.1	3968.1	7.2670
$p = 120 \text{ bar} = 12.0 \text{ MPa}$ ( $T_{\text{sat}} = 324.75^\circ\text{C}$ )					$p = 140 \text{ bar} = 14.0 \text{ MPa}$ ( $T_{\text{sat}} = 336.75^\circ\text{C}$ )			
Sat.	0.01426	2513.7	2684.9	5.4924	0.01149	2476.8	2637.6	5.3717
360	0.01811	2678.4	2895.7	5.8361	0.01422	2617.4	2816.5	5.6602
400	0.02108	2798.3	3051.3	6.0747	0.01722	2760.9	3001.9	5.9448
440	0.02355	2896.1	3178.7	6.2586	0.01954	2868.6	3142.2	6.1474
480	0.02576	2984.4	3293.5	6.4154	0.02157	2962.5	3264.5	6.3143
520	0.02781	3068.0	3401.8	6.5555	0.02343	3049.8	3377.8	6.4610
560	0.02977	3149.0	3506.2	6.6840	0.02517	3133.6	3486.0	6.5941
600	0.03164	3228.7	3608.3	6.8037	0.02683	3215.4	3591.1	6.7172
640	0.03345	3307.5	3709.0	6.9164	0.02843	3296.0	3694.1	6.8326
700	0.03610	3425.2	3858.4	7.0749	0.03075	3415.7	3846.2	6.9939
740	0.03781	3503.7	3957.4	7.1746	0.03225	3495.2	3946.7	7.0952

H<sub>2</sub>O

TABLE A-4 (Continued)

$T$ °C	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 160 \text{ bar} = 16.0 \text{ MPa}$ ( $T_{\text{sat}} = 347.44^\circ\text{C}$ )					$p = 180 \text{ bar} = 18.0 \text{ MPa}$ ( $T_{\text{sat}} = 357.06^\circ\text{C}$ )			
Sat.	0.00931	2431.7	2580.6	5.2455	0.00749	2374.3	2509.1	5.1044
360	0.01105	2539.0	2715.8	5.4614	0.00809	2418.9	2564.5	5.1922
400	0.01426	2719.4	2947.6	5.8175	0.01190	2672.8	2887.0	5.6887
440	0.01652	2839.4	3103.7	6.0429	0.01414	2808.2	3062.8	5.9428
480	0.01842	2939.7	3234.4	6.2215	0.01596	2915.9	3203.2	6.1345
520	0.02013	3031.1	3353.3	6.3752	0.01757	3011.8	3378.0	6.2960
560	0.02172	3117.8	3465.4	6.5132	0.01904	3101.7	3444.4	6.4392
600	0.02323	3201.8	3573.5	6.6399	0.02042	3188.0	3555.6	6.5696
640	0.02467	3284.2	3678.9	6.7580	0.02174	3272.3	3663.6	6.6905
700	0.02674	3406.0	3833.9	6.9224	0.02362	3396.3	3821.5	6.8580
740	0.02808	3486.7	3935.9	7.0251	0.02483	3478.0	3925.0	6.9623

$p = 200 \text{ bar} = 20.0 \text{ MPa}$ ( $T_{\text{sat}} = 365.81^\circ\text{C}$ )				
Sat.	0.00583	2293.0	2409.7	4.9269
400	0.00994	2619.3	2818.1	5.5540
440	0.01222	2774.9	3019.4	5.8450
480	0.01399	2891.2	3170.8	6.0518
520	0.01551	2992.0	3302.2	6.2218
560	0.01689	3085.2	3423.0	6.3705
600	0.01818	3174.0	3537.6	6.5048
640	0.01940	3260.2	3648.1	6.6286
700	0.02113	3386.4	3809.0	6.7993
740	0.02224	3469.3	3914.1	6.9052
800	0.02385	3592.7	4069.7	7.0544

$p = 240 \text{ bar} = 24.0 \text{ MPa}$			
0.00673	2477.8	2639.4	5.2393
0.00929	2700.6	2923.4	5.6506
0.01100	2838.3	3102.3	5.8950
0.01241	2950.5	3248.5	6.0842
0.01366	3051.1	3379.0	6.2448
0.01481	3145.2	3500.7	6.3875
0.01588	3235.5	3616.7	6.5174
0.01739	3366.4	3783.8	6.6947
0.01835	3451.7	3892.1	6.8038
0.01974	3578.0	4051.6	6.9567

$p = 280 \text{ bar} = 28.0 \text{ MPa}$				
400	0.00383	2223.5	2330.7	4.7494
440	0.00712	2613.2	2812.6	5.4494
480	0.00885	2780.8	3028.5	5.7446
520	0.01020	2906.8	3192.3	5.9566
560	0.01136	3015.7	3333.7	6.1307
600	0.01241	3115.6	3463.0	6.2823
640	0.01338	3210.3	3584.8	6.4187
700	0.01473	3346.1	3758.4	6.6029
740	0.01558	3433.9	3870.0	6.7153
800	0.01680	3563.1	4033.4	6.8720
900	0.01873	3774.3	4298.8	7.1084

$p = 320 \text{ bar} = 32.0 \text{ MPa}$			
0.00236	1980.4	2055.9	4.3239
0.00544	2509.0	2683.0	5.2327
0.00722	2718.1	2949.2	5.5968
0.00853	2860.7	3133.7	5.8357
0.00963	2979.0	3287.2	6.0246
0.01061	3085.3	3424.6	6.1858
0.01150	3184.5	3552.5	6.3290
0.01273	3325.4	3732.8	6.5203
0.01350	3415.9	3847.8	6.6361
0.01460	3548.0	4015.1	6.7966
0.01633	3762.7	4285.1	7.0372

H<sub>2</sub>O

H<sub>2</sub>O

TABLE A-5 Properties of Compressed Liquid Water

$T$ °C	$v \times 10^3$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K	$v \times 10^3$ m <sup>3</sup> /kg	$u$ kJ/kg	$h$ kJ/kg	$s$ kJ/kg · K
$p = 25 \text{ bar} = 2.5 \text{ MPa}$ ( $T_{\text{sat}} = 223.99^\circ\text{C}$ )					$p = 50 \text{ bar} = 5.0 \text{ MPa}$ ( $T_{\text{sat}} = 263.99^\circ\text{C}$ )			
20	1.0006	83.80	86.30	.2961	.9995	83.65	88.65	.2956
40	1.0067	167.25	169.77	.5715	1.0056	166.95	171.97	.5705
80	1.0280	334.29	336.86	1.0737	1.0268	333.72	338.85	1.0720
100	1.0423	418.24	420.85	1.3050	1.0410	417.52	422.72	1.3030
140	1.0784	587.82	590.52	1.7369	1.0768	586.76	592.15	1.7343
180	1.1261	761.16	763.97	2.1375	1.1240	759.63	765.25	2.1341
200	1.1555	849.9	852.8	2.3294	1.1530	848.1	853.9	2.3255
220	1.1898	940.7	943.7	2.5174	1.1866	938.4	944.4	2.5128
Sat.	1.1973	959.1	962.1	2.5546	1.2859	1147.8	1154.2	2.9202
$p = 75 \text{ bar} = 7.5 \text{ MPa}$ ( $T_{\text{sat}} = 290.59^\circ\text{C}$ )					$p = 100 \text{ bar} = 10.0 \text{ MPa}$ ( $T_{\text{sat}} = 311.06^\circ\text{C}$ )			
20	.9984	83.50	90.99	.2950	.9972	83.36	93.33	.2945
40	1.0045	166.64	174.18	.5696	1.0034	166.35	176.38	.5686
80	1.0256	333.15	340.84	1.0704	1.0245	332.59	342.83	1.0688
100	1.0397	416.81	424.62	1.3011	1.0385	416.12	426.50	1.2992
140	1.0752	585.72	593.78	1.7317	1.0737	584.68	595.42	1.7292
180	1.1219	758.13	766.55	2.1308	1.1199	756.65	767.84	2.1275
220	1.1835	936.2	945.1	2.5083	1.1805	934.1	945.9	2.5039
260	1.2696	1124.4	1134.0	2.8763	1.2645	1121.1	1133.7	2.8699
Sat.	1.3677	1282.0	1292.2	3.1649	1.4524	1393.0	1407.6	3.3596
$p = 150 \text{ bar} = 15.0 \text{ MPa}$ ( $T_{\text{sat}} = 342.24^\circ\text{C}$ )					$p = 200 \text{ bar} = 20.0 \text{ MPa}$ ( $T_{\text{sat}} = 365.81^\circ\text{C}$ )			
20	.9950	83.06	97.99	.2934	.9928	82.77	102.62	.2923
40	1.0013	165.76	180.78	.5666	.9992	165.17	185.16	.5646
80	1.0222	331.48	346.81	1.0656	1.0199	330.40	350.80	1.0624
100	1.0361	414.74	430.28	1.2955	1.0337	413.39	434.06	1.2917
140	1.0707	582.66	598.72	1.7242	1.0678	580.69	602.04	1.7193
180	1.1159	753.76	770.50	2.1210	1.1120	750.95	773.20	2.1147
220	1.1748	929.9	947.5	2.4953	1.1693	925.9	949.3	2.4870
260	1.2550	1114.6	1133.4	2.8576	1.2462	1108.6	1133.5	2.8459
300	1.3770	1316.6	1337.3	3.2260	1.3596	1306.1	1333.3	3.2071
Sat.	1.6581	1585.6	1610.5	3.6848	2.036	1785.6	1826.3	4.0139
$p = 250 \text{ bar} = 25 \text{ MPa}$					$p = 300 \text{ bar} = 30.0 \text{ MPa}$			
20	.9907	82.47	107.24	.2911	.9886	82.17	111.84	.2899
40	.9971	164.60	189.52	.5626	.9951	164.04	193.89	.5607
100	1.0313	412.08	437.85	1.2881	1.0290	410.78	441.66	1.2844
200	1.1344	834.5	862.8	2.2961	1.1302	831.4	865.3	2.2893
300	1.3442	1296.6	1330.2	3.1900	1.3304	1287.9	1327.8	3.1741